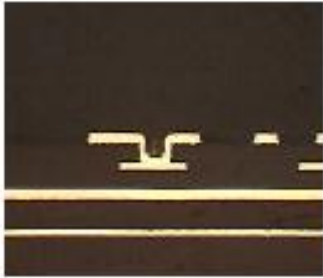


**Speaker is an invited presentation  
A **Technical Paper** was not required for  
the 2014 APEXPO™ Technical  
Conference**

# **The Total Environmental Solution for Any-layer HDI Production**

Steven Tam, Andreas Gloeckner, Christian Rietmann  
Enthone Inc.



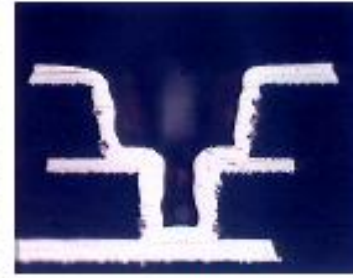
Blind Via



Stagger Via



Skip Via



Stack Via  
(Step type)



Stack Via  
(Cu fill)



1+N+1 HDI Structure



2+N+2 Stacked Via Structure



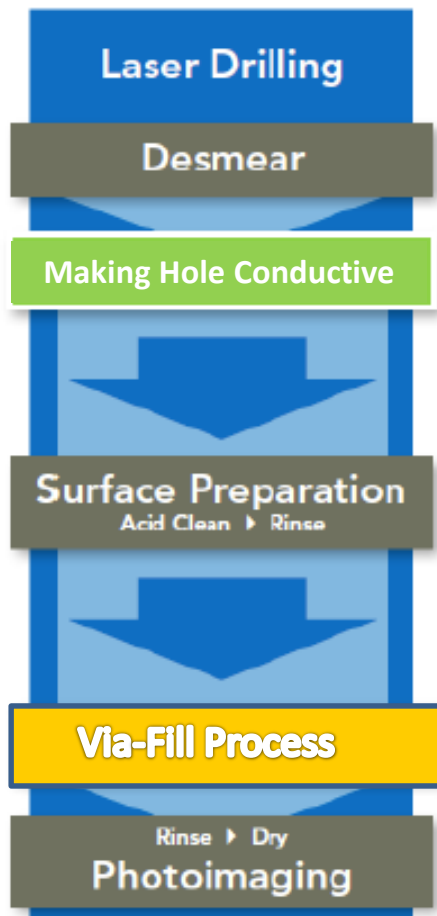
3+N+3 Stacked Via Structure



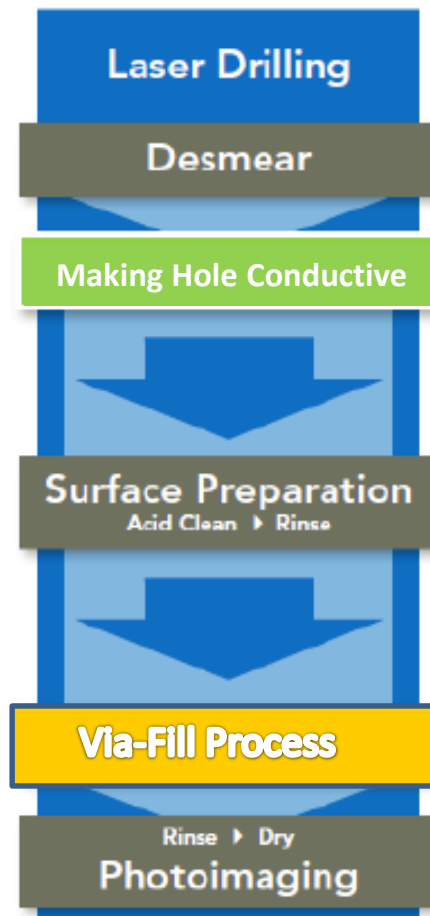
Any Layer Structure

## Overview of different Via-Fill Technology

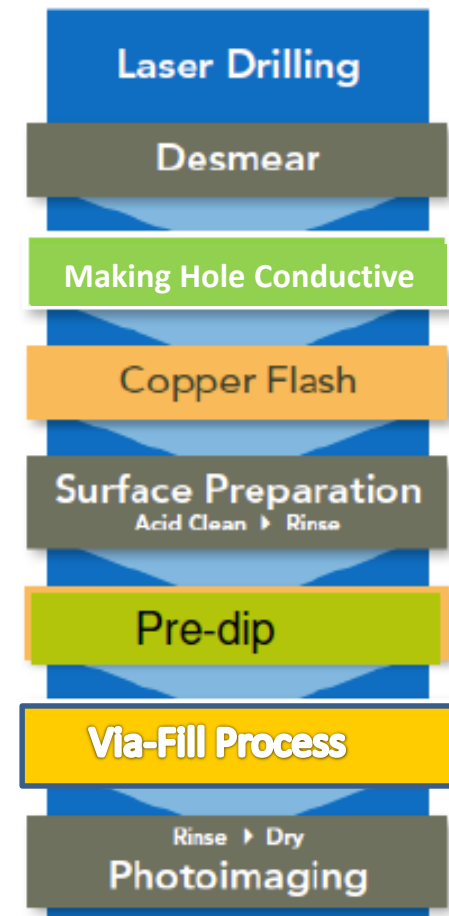
### Super-Filling



### Partial-Filling



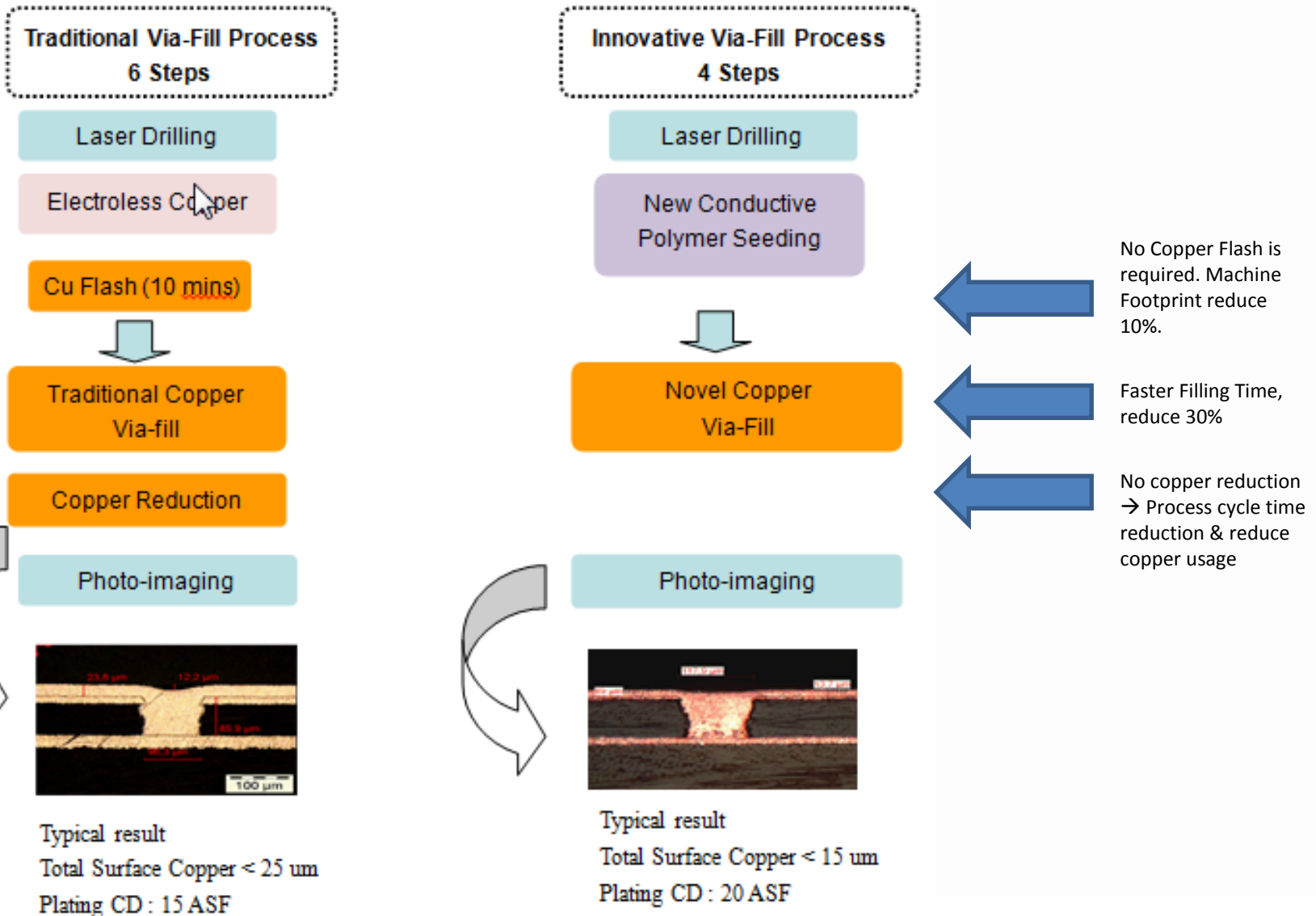
### Conventional Filling





# NEW IDEAS ... FOR NEW HORIZONS

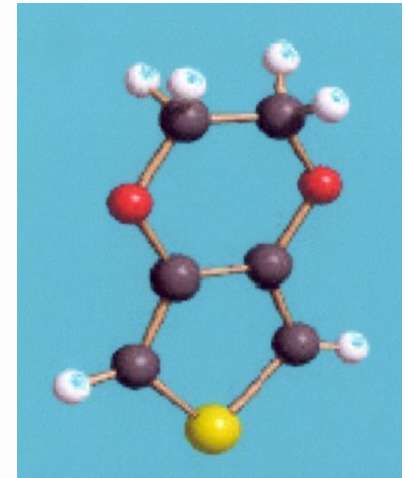
## Process Value of new developed Via-Fill Process



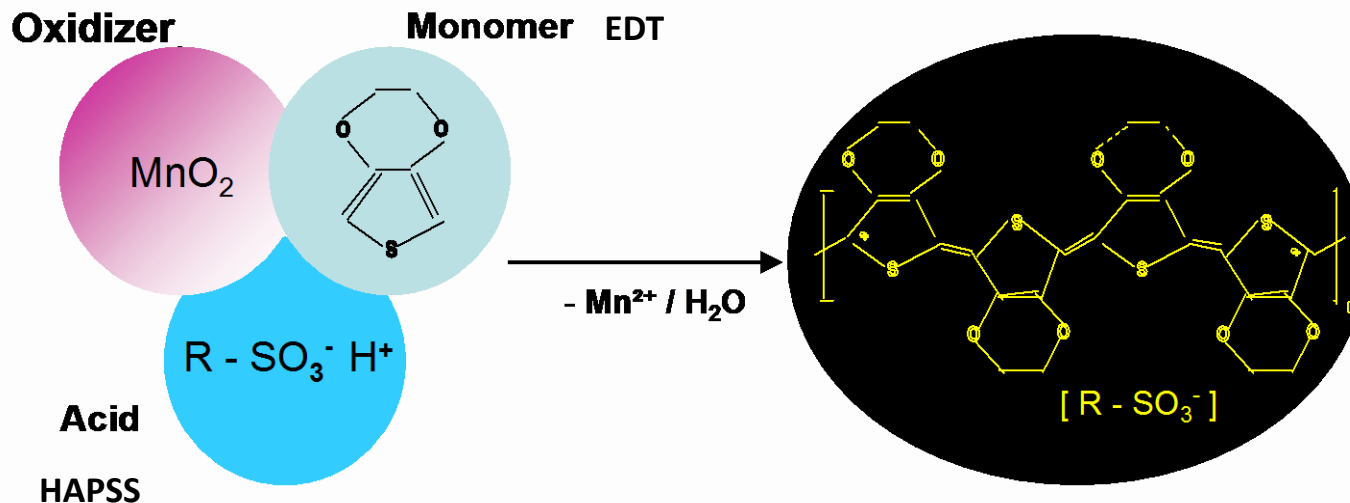
## Conductive Polymer Mechanism

- Reaction Mechanism Simplified**

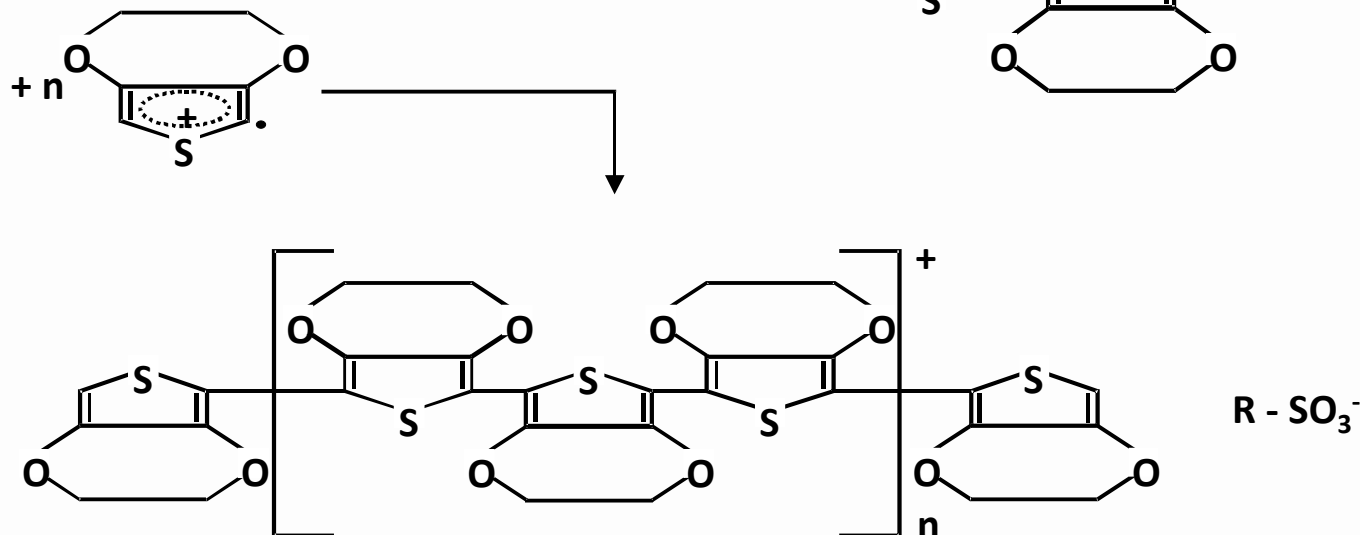
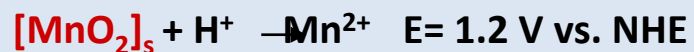
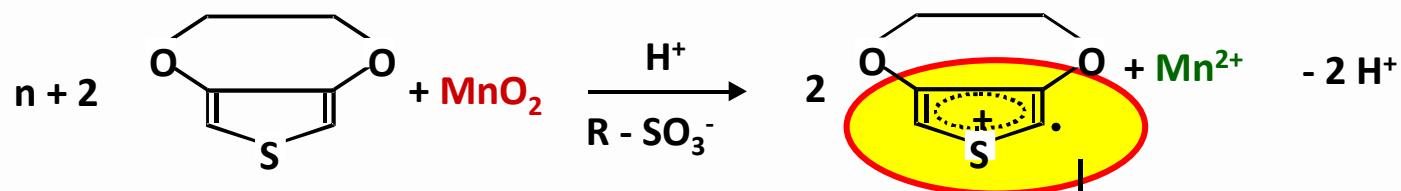
- Activation of Dielectrics only
  - Selective  $\text{MnO}_2$  formation (Initiator)
- Polymerization of
  - Monomer - EDT
  - Organic Sulfonic Acid - HAPSS



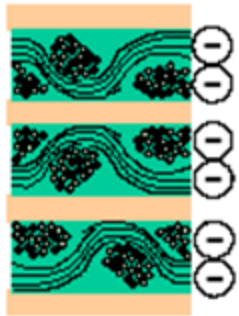
Corner Stone: EDT



## Reaction mechanism

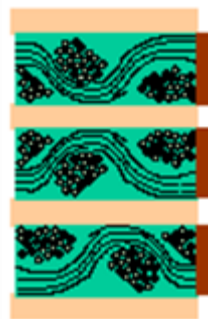


## Formation of Conductive Polymer



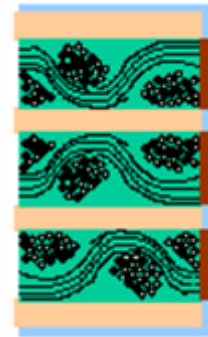
Step 1  
Conditioner

Cationic polymer  
improves MnO<sub>2</sub>  
absorption



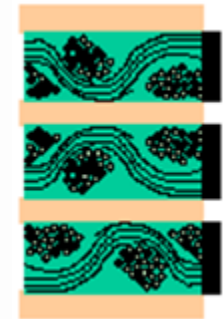
Step 2  
Initiator  
Permanganate treatment

Selective MnO<sub>2</sub>  
Deposition on  
Glass and resin



Step 3  
Catalyst  
Polymerization

EDT monomer  
coats MnO<sub>2</sub> and is  
oxidized in the  
presence of PSS  
PSS donates H<sup>+</sup>  
ions making the  
coating conductive



Conductive Polymer

This selective properties of Conductive Polymer can be proven by analytical techniques.



## Properties Of Conductive Polymer

- **Appearance**
  - Uniformly Dark Greenish to Anthracite/Black
  - Thickness approximately 100nm
- **Characteristics**
  - High Mechanical Stability
  - Thermal Stability (400° C)
  - Resistance approx. 5 K $\Omega$  / inch
- **Stability**
  - Sensitive to Chemical Oxidation (or Reduction)
  - Marginal loss of Conductivity
    - Storage Dependent (4-5 Days Guaranteed)

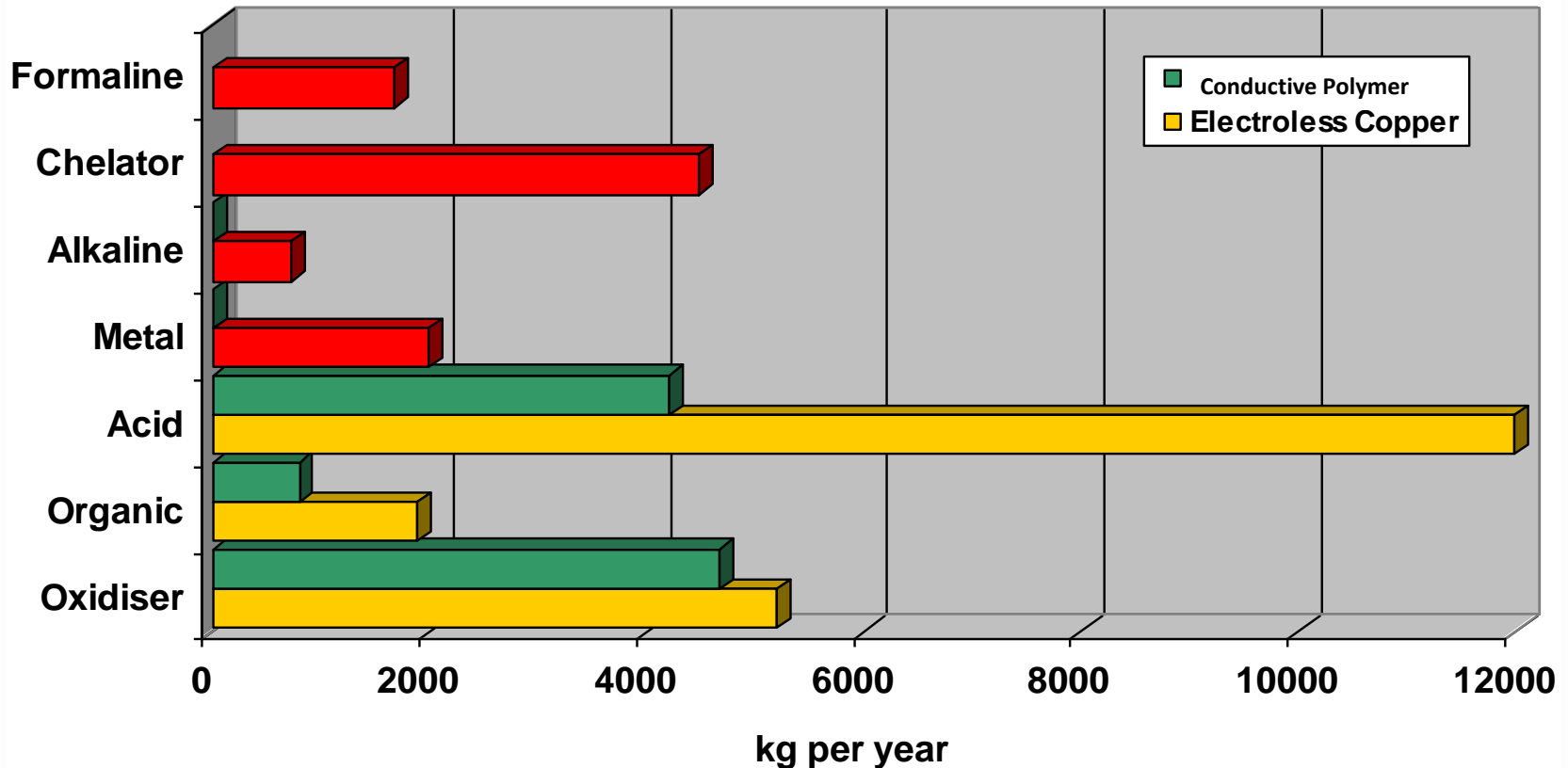
# Environmental Benefits

## Environmental friendly

### **No chelators, No formaldehyde**

- Improved worker's health
- Reduced waste generation
- Reduced water and energy consumption
- Simplified waste water treatment
- Lower water consumption
- **Lower costs**

## Cumulative Consumption of Chemicals per Year



400 000 m<sup>2</sup> Laminate / Year, horizontal

## Cumulative Consumption of Chemicals per Year

	Typical Electroless Copper	Conductive Polymer
Oxidizing Agents	5200 kg	4680 kg
Acid	14148 kg	4180 kg
Organic	1864 kg	784 kg
Metal	2008 kg	-
Alkaline	720 kg	-
Chelator	4480 kg	-
Formaldehyde	1680 kg	-

Based on: Horizontal Drag Out 80mL/L, 400,000 m<sup>2</sup> board per year



## **Direct Metallization**

### **Alternatives to Electroless Copper (E'Cu)**

- **Direct Metallization**
  - Pd Seeding
    - Activation on Dielectrics & Copper Surfaces
    - Etch-Back Removal of Activated Copper Surfaces
  - Graphite- & Carbon Activation
    - Activation on Dielectrics & Copper Surfaces
    - Etch-Back Removal of Activated Copper Surfaces
  - Intrinsic Conductive Polymer (ICP)
    - **Activation of Dielectrics Only**
    - **Without Etch-Back Removal of Activated Copper Surfaces**

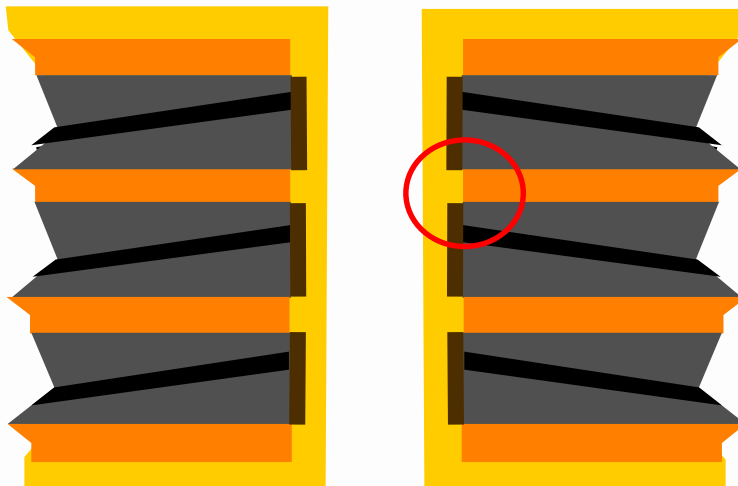
## Importance of Selective Activation

- **Selective Activation**

- Performance Reliability
- Only Dielectrics

Laminate Resin

Glass Reinforcement



**No Inner Connect Defect**

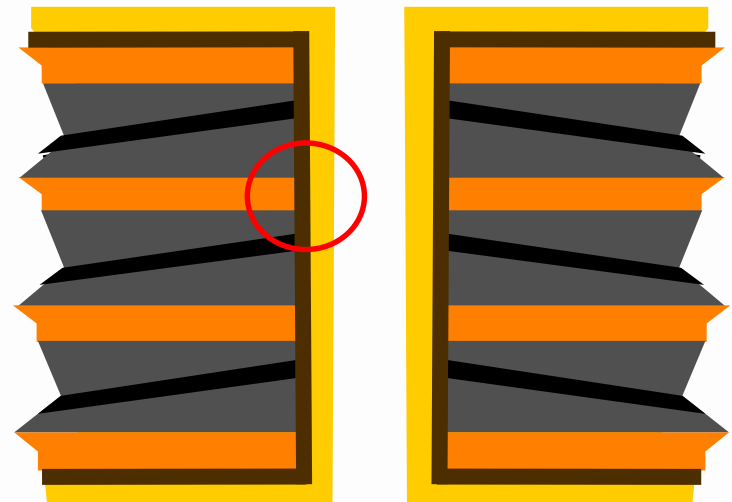
- **Non-Selective Activation**

- Performance Failure
- Total Surface Activation

Laminate Resin

Glass Reinforcement

Copper Surface



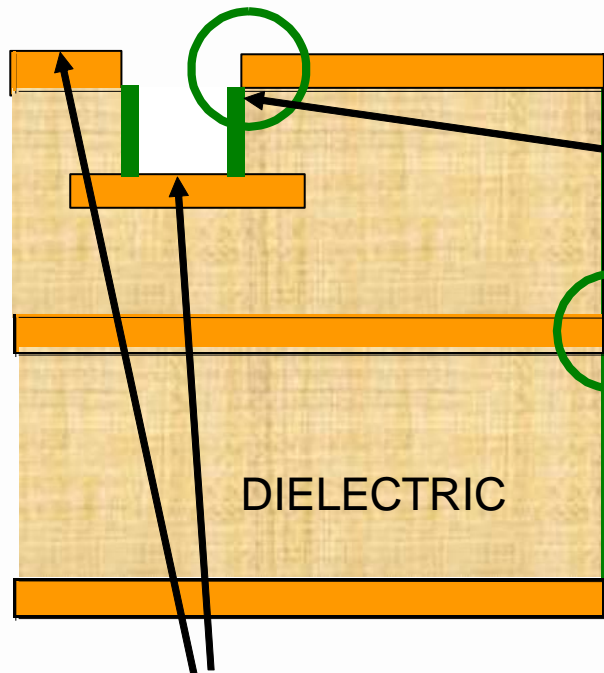
**Inner Connect Defect Risk**

**Activation on Copper must be removed chemically with risk**

**Conductive  
Polymer**

**(needs no microetch)**

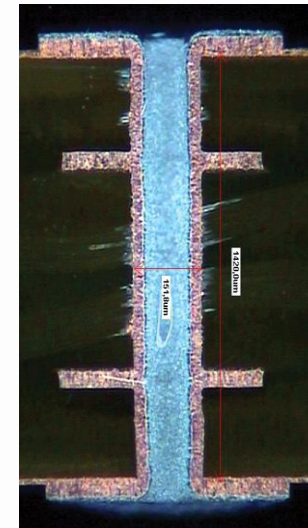
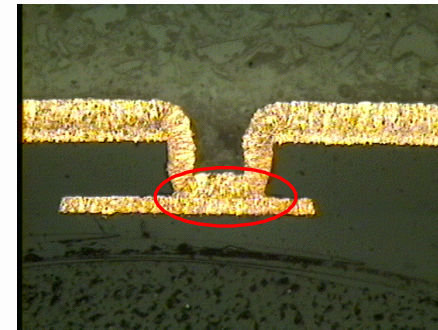
**Complete Coverage of  
Micovias and Inner Layers**

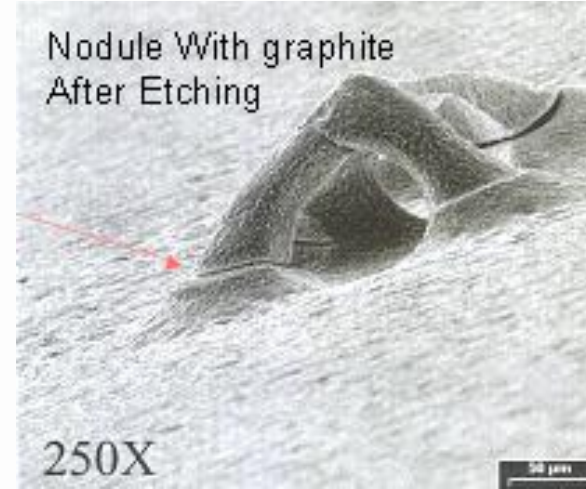
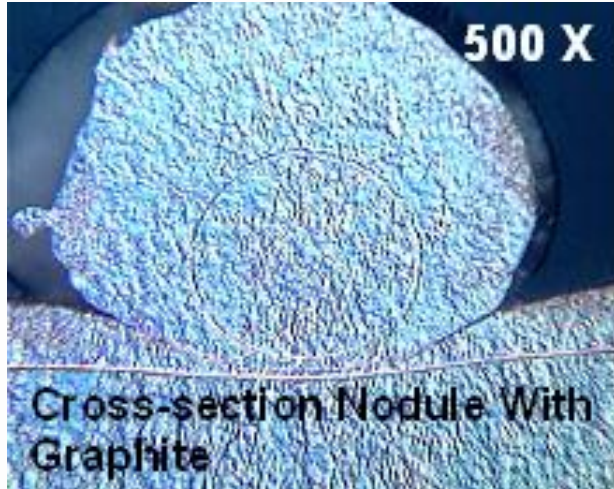


**No Etch  
removal  
of copper  
at critical  
points**

**Conductive  
Polymer  
(only on  
dielectric)**

**No material deposited on Via  
capture pad or surface copper**



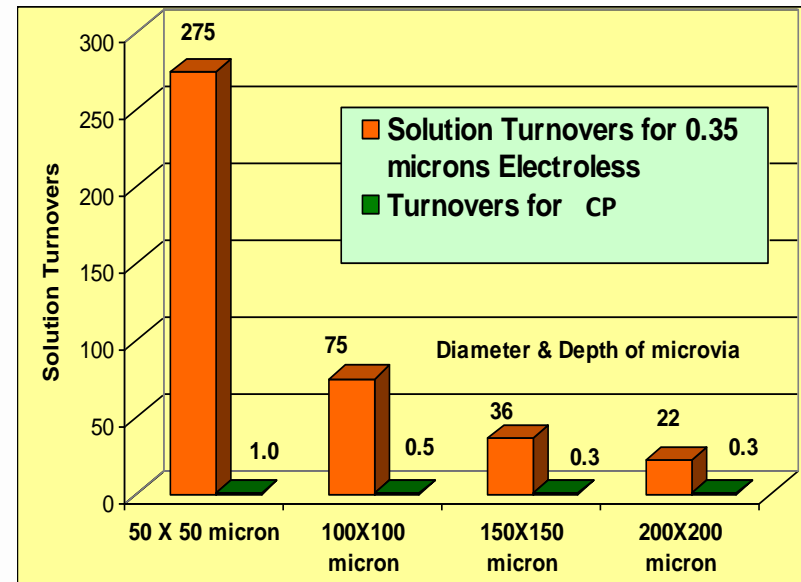
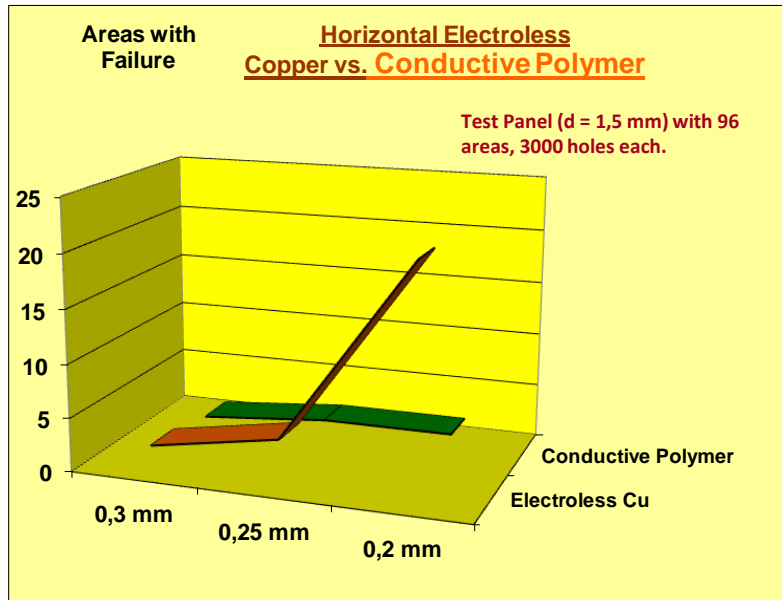


Nodules generated on copper surface with graphite, resulting in rough copper plating

- **The post-etching is needed in non-selective process**
  - There is negative etchback issue from over etching
  - Add a waste etchant solution treatment
- **Roller residues from carbon or graphite often cause rough deposits and quality issue in line manufacturing**



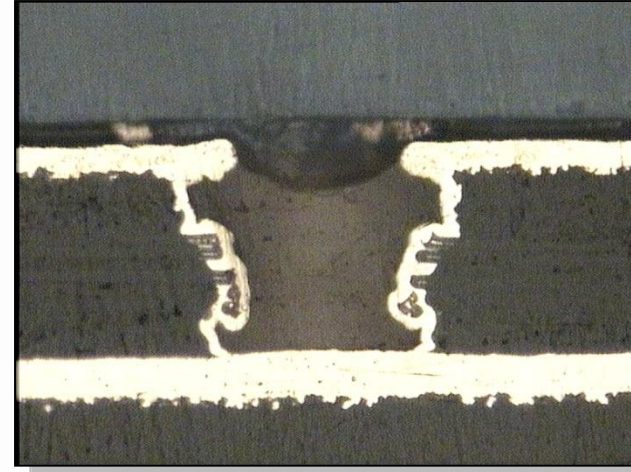
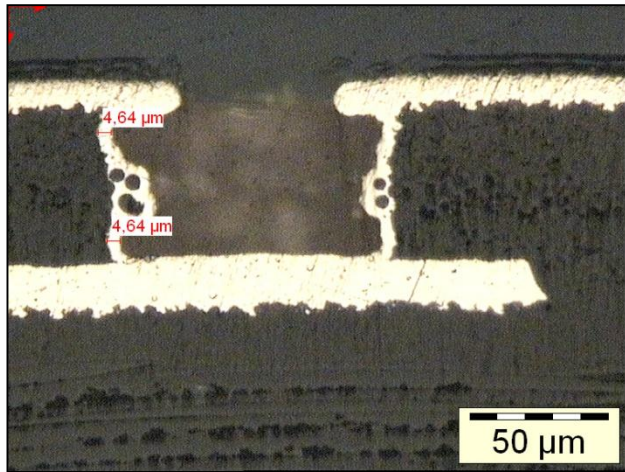
## Process Reliability



### WHY is Conductive Polymer better for Microvias?

1. Easy to Conveyorize
2. Low Viscosity of Process Solutions
3. Chemical Bond to Dielectric Material
4. No H<sub>2</sub> Formation During Plating Process
5. Minimal Solution Exchange Required to Deposit Conductive Polymer

## Glass fibre coverage



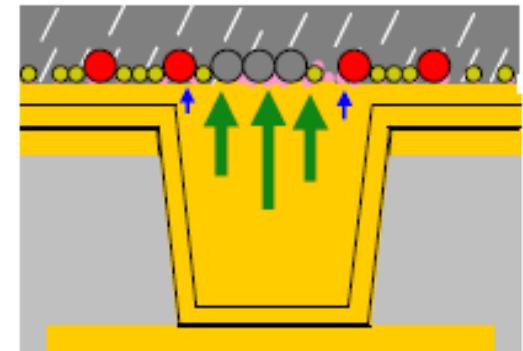
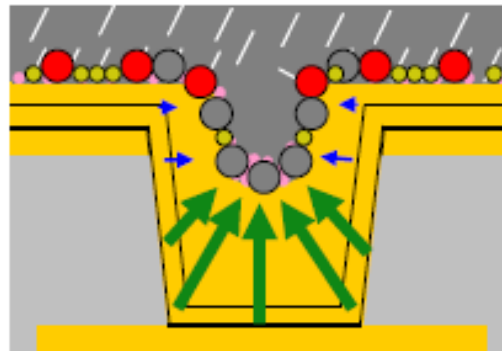
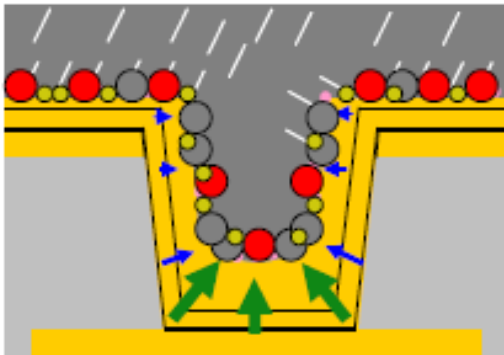
### Copper Coverage after Initial Via-Fill Plating at 2 ASD for 10 minutes

- With a high copper and a low acid concentration, the initial copper plating starts relative easy.
- Conductive Polymer help a good copper coverage on glass and resin.
- A copper layer is formed and the adsorption/desorption of the inhibitor/accelerator system can take place.

## Via- Filling mechanism

### Innovative Via-Filling

- Inhibitor/Suppressor + ● Chloride suppresses plating rate
- Brightener / Activator
- Leveler



- Inhibitor/Suppressor
- Brightener/Activator
- Leveler

#### Cu<sup>2+</sup> concentration

Higher concentration support better filling performance

#### H<sup>+</sup> concentration

Enhance conductivity of solution

#### Cl<sup>-</sup> concentration

Ingredient for brightener & carrier intermediates

#### Carrier

Formation of diffusion layer, reduce surface tension

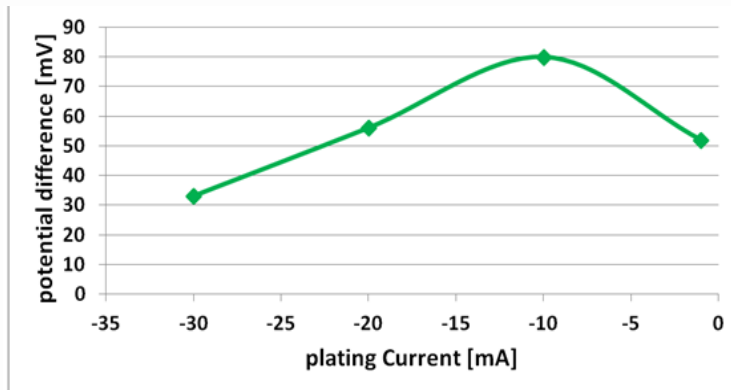
#### Accelerator

Grain refiner for copper deposit

#### Leveler

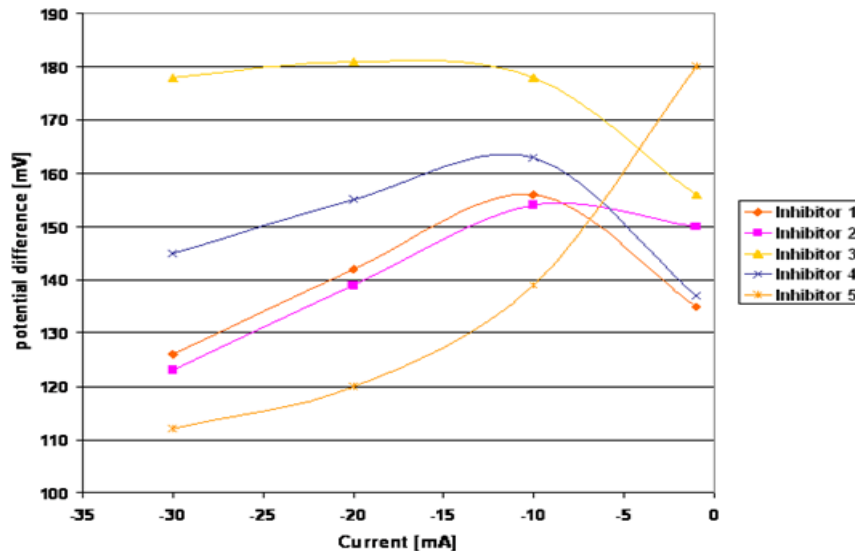
Provide micro-leveling effect for copper deposition

# Electrochemical Study



## Best Plating Window

- Additive set had the biggest influence on plating between -10 mA to -20mA.
- The best current density range for plating with the development solution is in the range of 1 to 2 ASD.

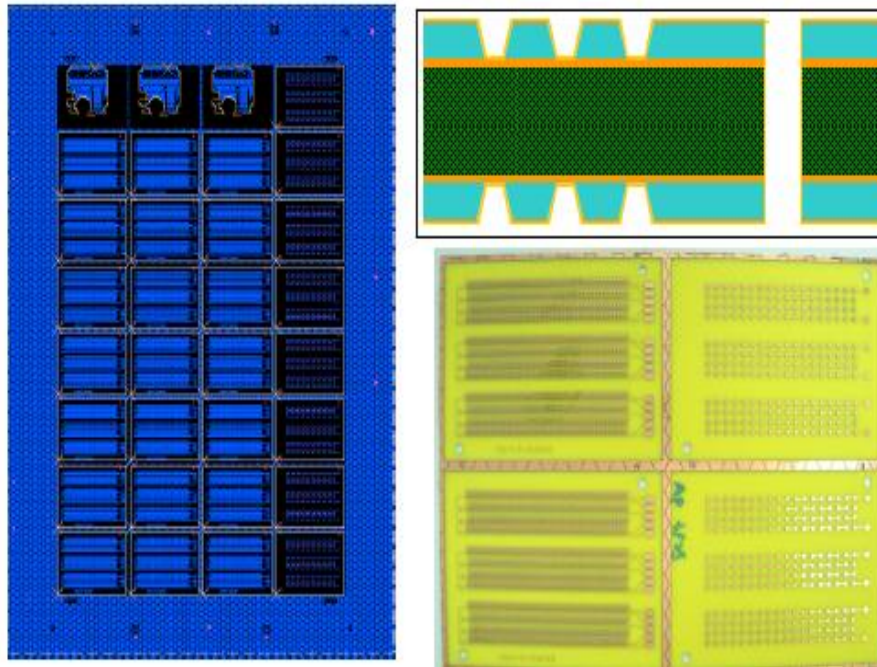


## Testing with different inhibitor/accelerator systems.

- The inhibitor systems 1, 2 and 4 have a similar curve.
- Inhibitor 3 system shows conformal filling in the working window of 1 to 2 ASD.
- Inhibitor 5 gives good filling but the plating time is lower and the overburden is higher.



# Test Vehicle Description



It is a 4 layer daisy chain design with 100 and 125  $\mu\text{m}$  via and 250, 300 and 350 mm through hole. Core was 500  $\mu\text{m}$  (20mil) 1/1 with 1080PP with 65% RC. Final HDI layer dielectric thickness was approximately 60  $\mu\text{m}$ . There was no control on direct laser drill as the intention was to check the coating performance if micro-via quality was poor. Example of poor quality is overhang and large glass fiber protrusion.

## Plating Tool Type

### *Plating tool configuration A - Low Flow System*

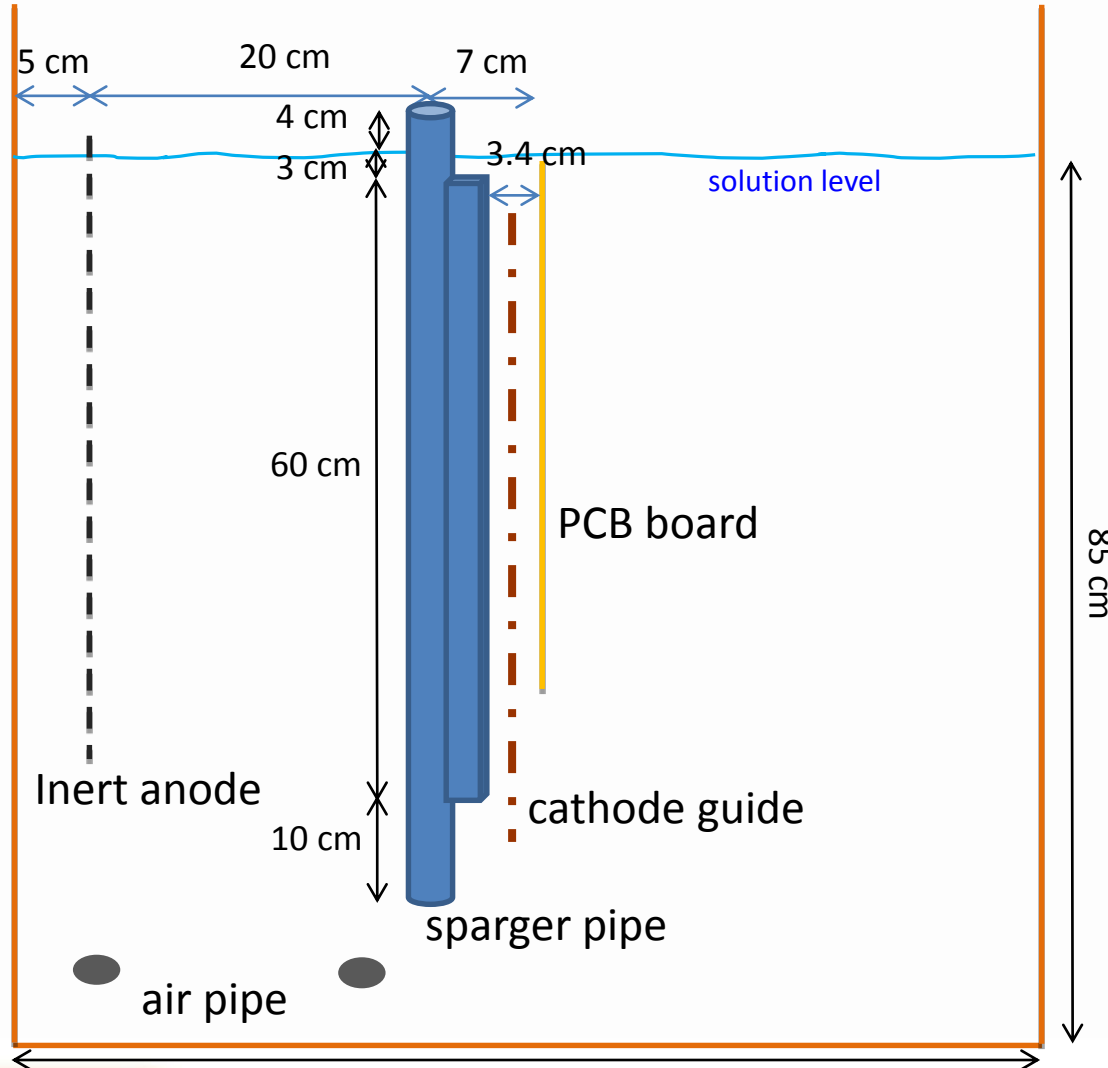
- Immersion type, where the boards are moving between two sparger systems on both side.
- The air agitation is optional; however, the flow rate of the solution could be adjusted from low to high, depending on the preference of the hydrodynamic flow required for the additive.
- In this set up the additive control becomes the predominate factor for via-filling, rather than solution flooding.

### *Plating tool configuration B -High Flow System*

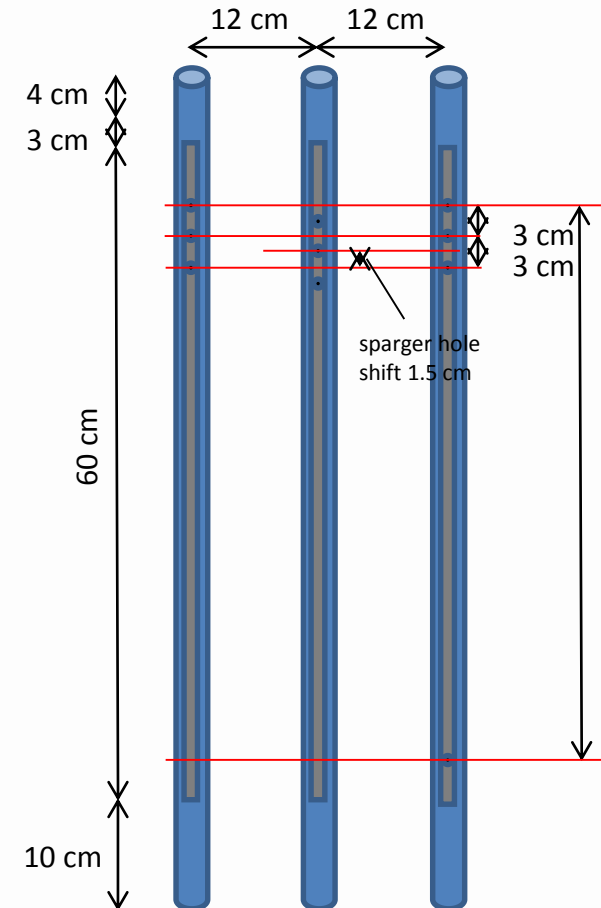
- Strong flooding design where the solution level is maintain under a high flow pressure.
- It helps the solution exchange within the micro via by forced flooding. Via-fill mechanism is dominated by hydrodynamic flow.

## Plating Tool – Type A

**Copper plating tank (side view)**

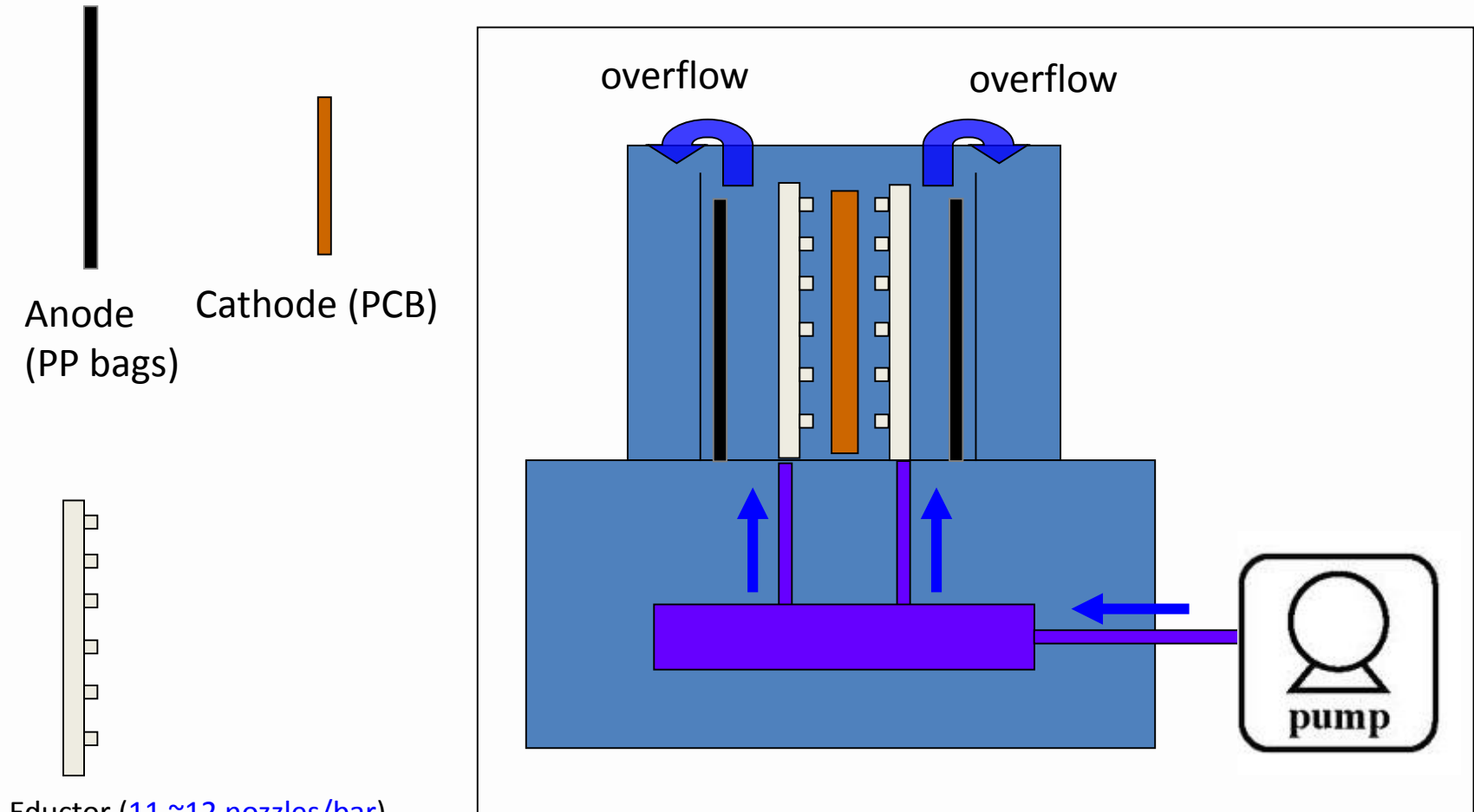


**Sparger pipe**



## Plating Tool – Type B

Plating line side view



Eductor (11 ~12 nozzles/bar)

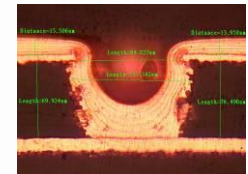
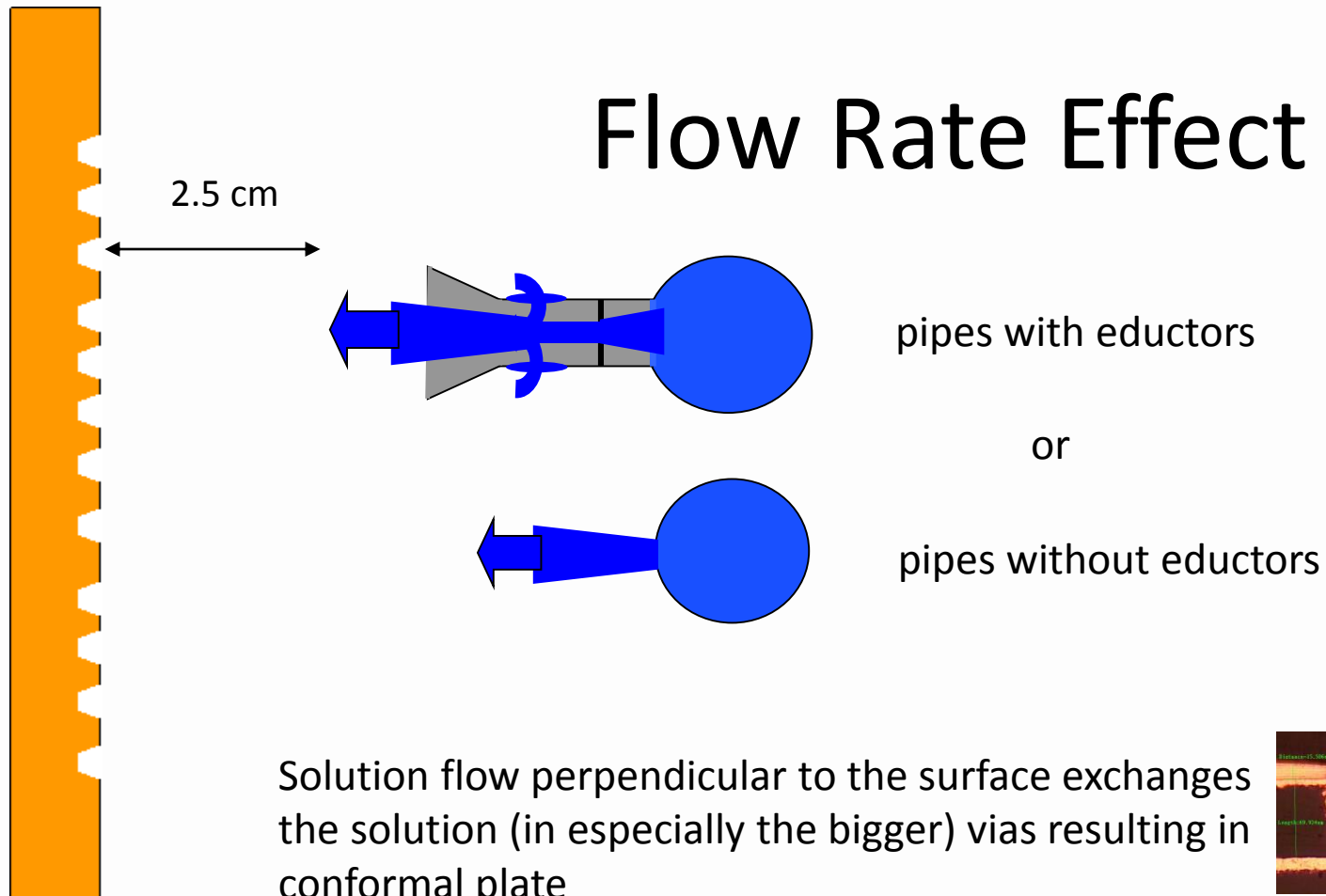
1 set has 8 bars, 1 plating side has 6 sets

**No air agitation**



# Hydrodynamic Study

## Flow Rate Effect

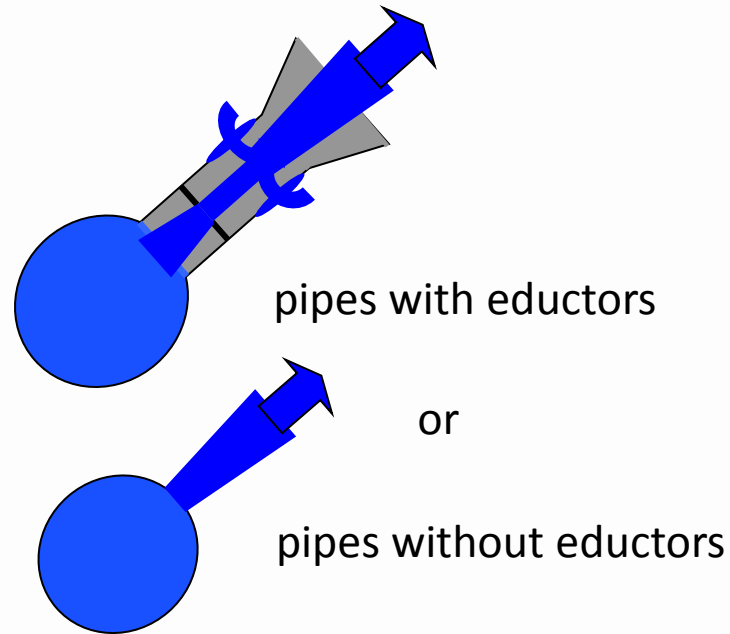


# Flow Rate Effect

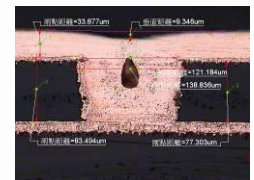
Cathode  
with vias



Little  
solution  
agitation  
at  
surface;  
copper  
ion  
diffusion  
into vias  
is limited



Pipe openings turned away from surface resulting in  
good fill, butt centre / top voids.

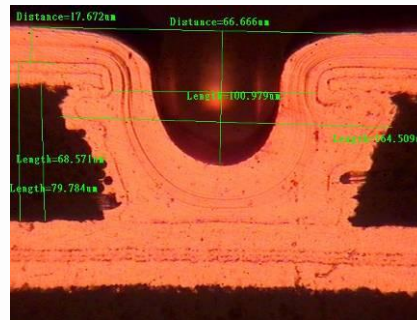
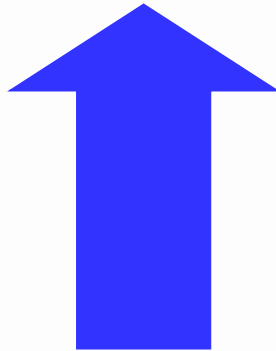


# Flow Rate Effect

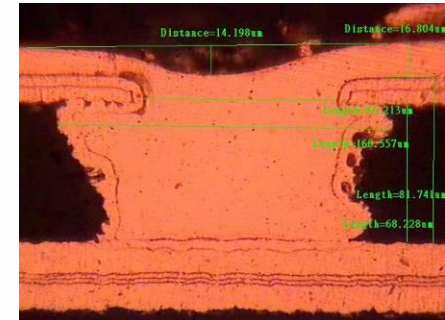
Solution  
flow  
along the  
surface is  
needed

Air agitation would have supplied the right solution flow  
along the surface. This does not add fresh leveler into  
the vias and provides good copper ion diffusion into  
them.

Cathode  
with vias



panel plated in AEL  
tool



panel plated in haring cell  
with air agitation

## Sparger Flowrate Profile (use of **High** flowrate)

Higher flowrate can enhance the solution exchange inside the BMV (Blind Micro-Via) especially at the BMV bottom or the deep BMV.

Higher flowrate is required for the BMV will poor laser drilling, the solution exchange is generally poor with overhang or glass fiber protrusion.

Higher flowrate may cause the strong solution turbulence inside the BMV that cause the unstable diffusion layer (of the electroplating chemistry). The brightener (accelerator) may be “washed” away and cannot perform the bottom-up BMV filling reaction. At the same time, the Leveler flush into the BMV (as well as the surface copper) that suppress the copper growth inside the BMV.

Too high flowrate (keep for the whole plating period) may cause larger dimple.

Generally speaking,

- deep BMV needs higher flowrate
- at the beginning of the plating needs higher flowrate

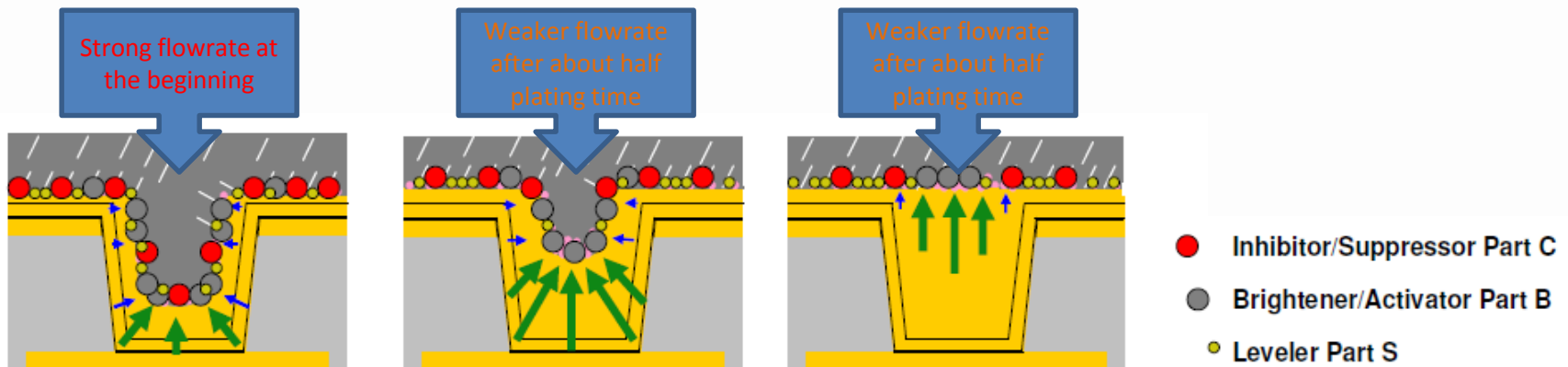
## Sparger Flowrate Profile (use of **Low** flowrate)

Low flowrate can give more stable diffusion layer (of electroplating chemistry), the brightener (accelerator) is more stable inside the BMV and stick on the hole wall copper and give bottom-up copper plating.

Low flowrate can be used for the shallow BMV (e.g. 50 um depth).

Low flowrate is more suitable for the larger diameter BMV, as the solution exchange is already easier. If flowrate is high, the brightener in the diffusion will be unstable → less bottom-up plating → larger dimple.

Low flowrate is more suitable to used after half of the total plating time.



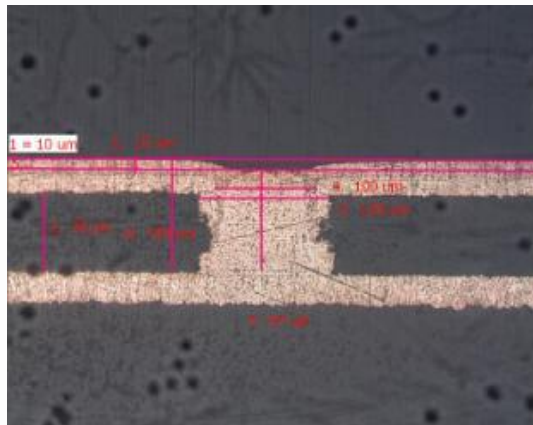


## Current Density Profile Study

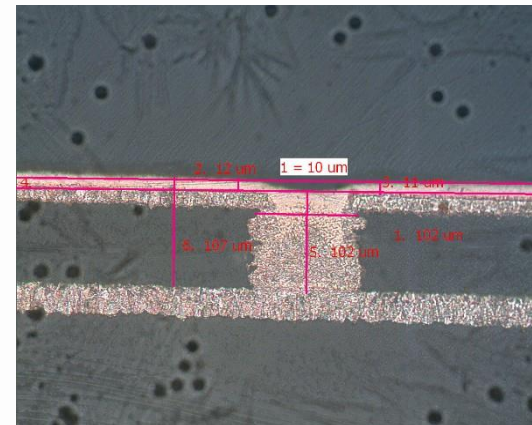
Flash panel layer has the best conductivity among all the conductive layers

Flash panel layer may starts with 1.5 ASD. And keep the same current density plate to the end.

On the other hand, to shorten the plating time or increase the surface copper thickness (according to the production specification), ramp current can be applied.



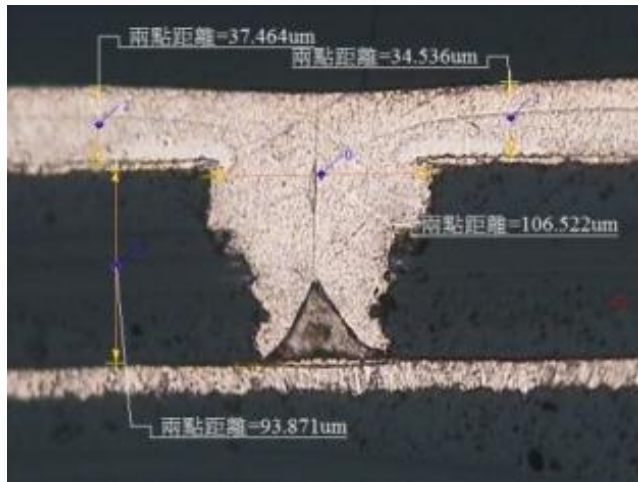
**1.5 ASD x 60 min**



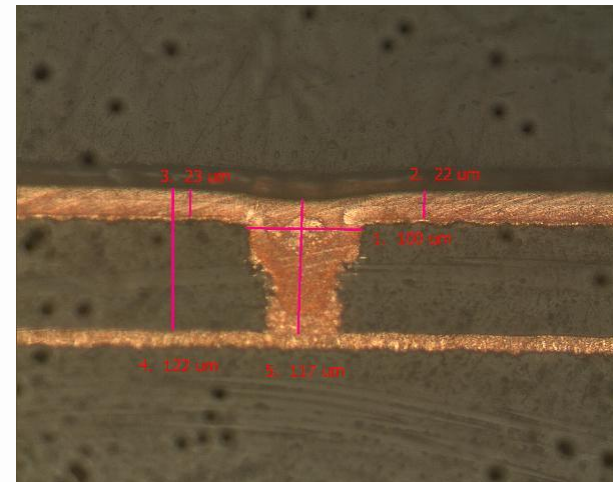
**1.5 ASD x 40 min +  
2.5 ASD x 10 min  
Total 50 min**

## Current Density Profile (cont')

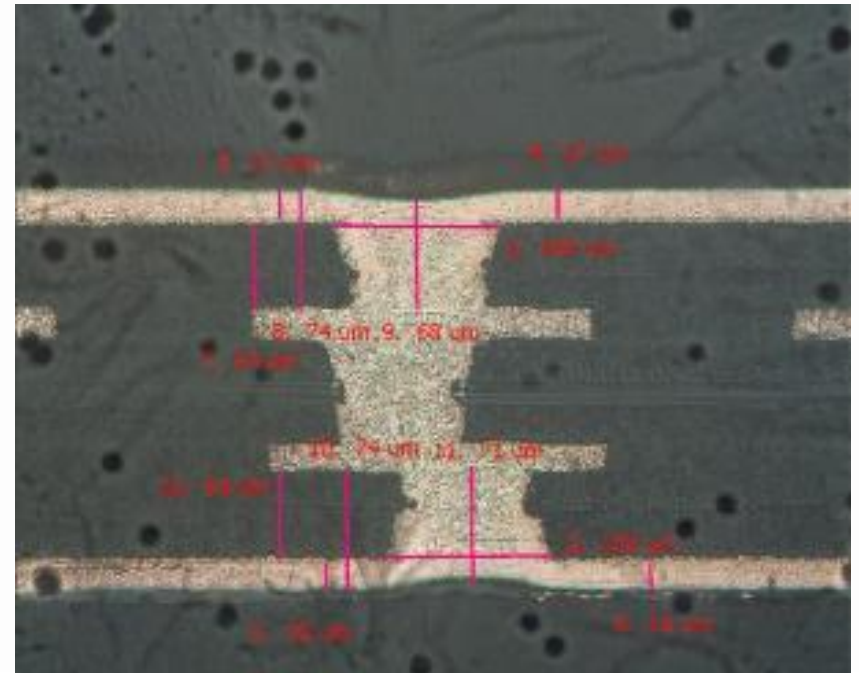
For direct metallization seeding, starts with 3 ASD x 5 min is recommended, the higher current density at the beginning can overcome the resistant barrier of the conductive layers. Longer high current density is not recommended because the surface copper and BMV top corner will plate too thick copper that increase the chance of void or liquid inclusion. The following is the example for 4 mil diameter/4 mil depth BMV.



**3 ASD x 20 min** (@ 12000 L/hr) +  
2 ASD x 20 min (@ 10000 L/hr) +  
4 ASD x 17 min (@ 7000 L/hr)



**3 ASD x 5 min** (@ 12000 L/hr) +  
1.2 ASD x 50 min (@ 12000 L/hr) +  
1.5 ASD x 35 min (@ 7000 L/hr)



## Via-Filling Performance at Tool A

Conductivity Layer	Direct Metallization
Current density	3 → 1.2 → 1.7 ASD
Plating time	120 min
Sparger flowrate (for every 2 m length)	12000 → 8000 L/hr

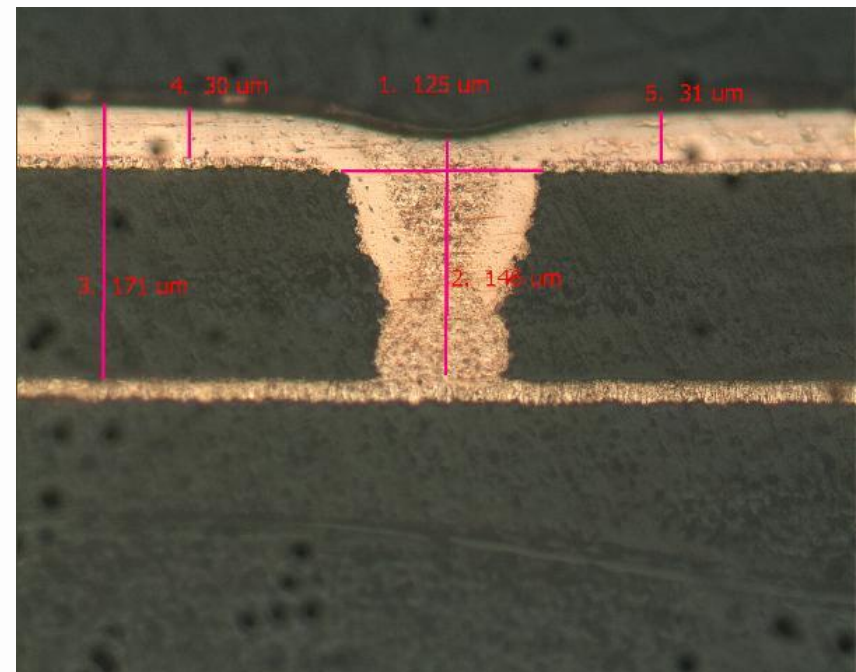
Customer "C" (special application)

Ø135 µm

Depth: 5 mil

Surface copper: ~30 µm

Dimple: <25 µm





## Via-Filling Performance at Tool A

Conductivity Layer	Direct Metallization
Current density	3 → 1.2 → 1.5 ASD
Plating time	90 min
Sparger flowrate (for every 2 m length)	12000 → 7000 L/hr

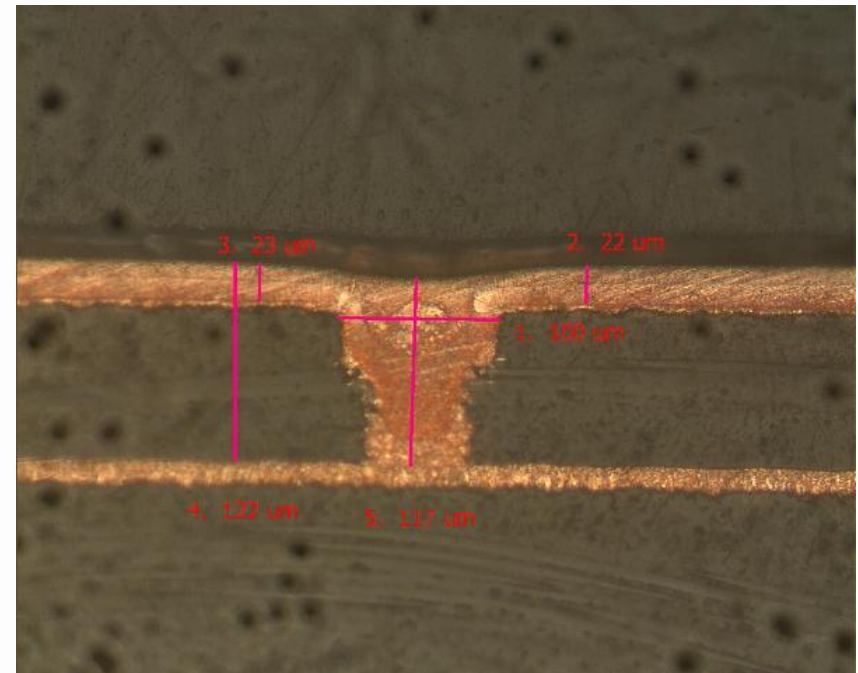
Customer "C" (special application)

Ø4 mil

Depth: 92 µm

Surface copper: 16 µm

Dimple: ~13 µm

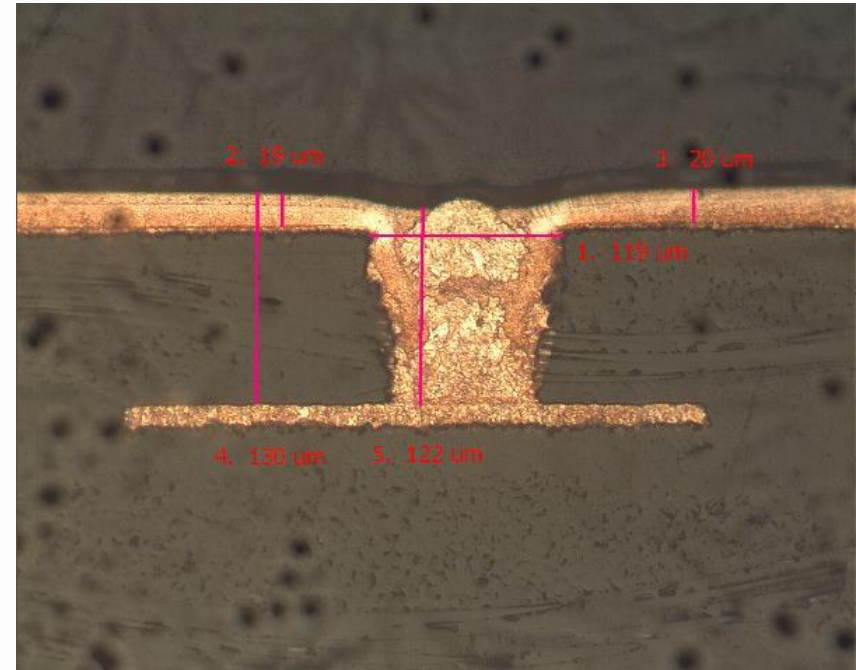




## Via-Filling Performance at Tool A

Conductivity Layer	Direct Metallization
Current density	3 → 1.2 → 1.5
Plating time	85 min
Sparger flowrate (for every 2 m length)	12000 → 7000 L/hr

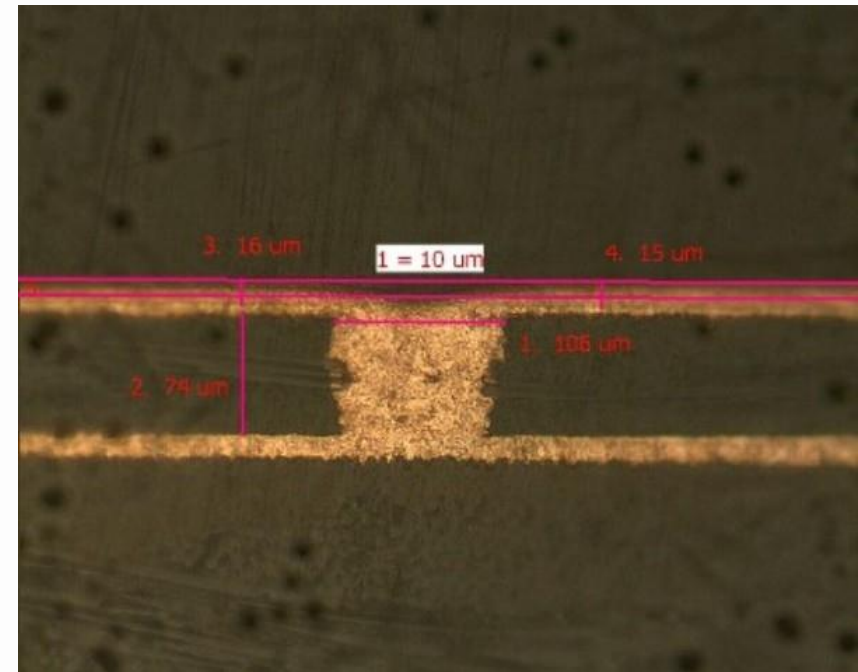
Customer "D" test board  
 Ø4 mil  
 Depth: 4 mil  
 Surface copper: 19 µm  
 Dimple: 8 µm



## Via-Filling Performance at Tool A

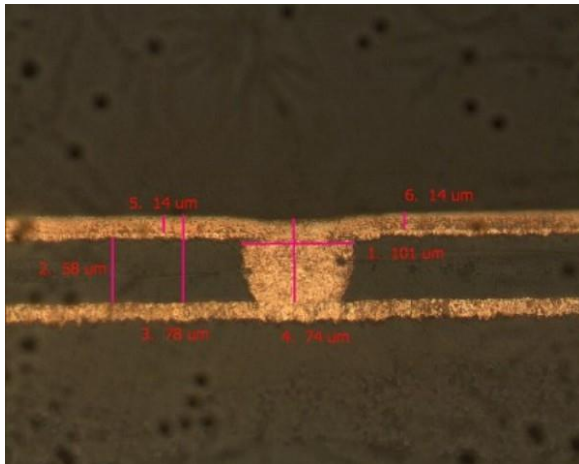
Conductivity Layer	Direct Metallization
Current density	3 → 1.5 → 2.2 ASD
Plating time	45 min
Sparger flowrate (for every 2 m length)	10000 → 8000 → 5000 L/hr

Ø4 mil  
 Depth: 3 mil  
 Surface copper: 13 um  
 Dimple: 10 um

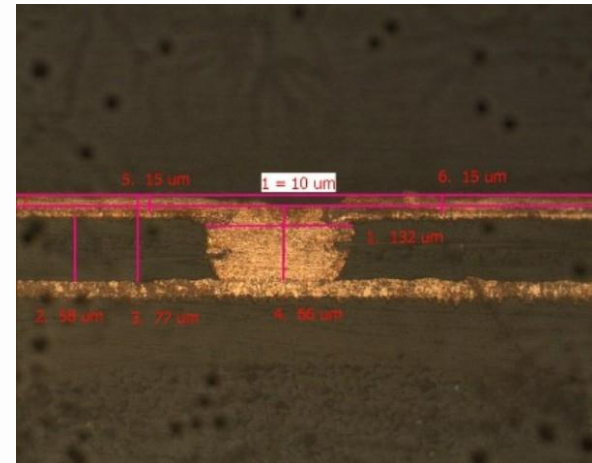


## Via-Filling Performance at Tool A

Conductivity Layer	Direct Metallization
Current density	3→1.5→2.2 ASD
Plating time	45 min
Sparger flowrate (for every 2 m length)	10000→ 8000→ 5000 L/hr



Ø4 mil  
Depth: 2 mil  
Surface copper: 14 um  
Dimple: 1 – 4 um

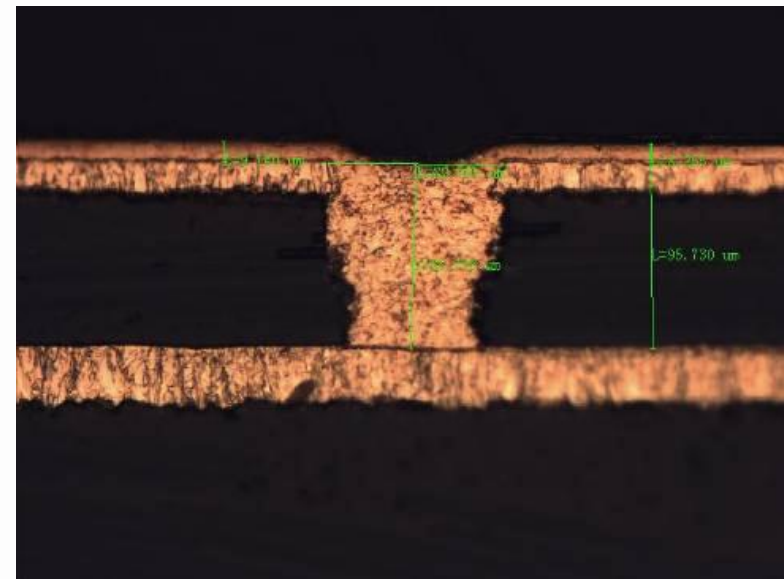


Ø5 mil  
Depth: 2 mil  
Surface copper: 15 um  
Dimple: ~10 um

## Via-Filling Performance at Tool A

Conductivity Layer	Direct Metallization
Current density	1.5 ASD
Plating time	50 min
Sparger flowrate	10 L/ft <sup>2</sup>

Ø80 µm  
 Depth: 85 µm  
 Surface copper: 9 µm  
 Dimple: <15 µm





## Via-Filling Performance at Tool A

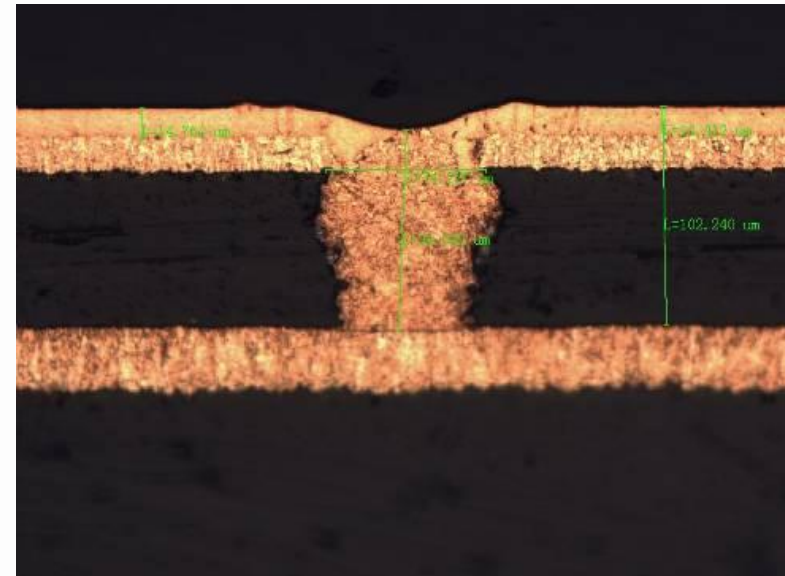
Conductivity Layer	Direct Metallization
Current density	2.5 ASD
Plating time	40 min
Sparger flowrate	10 L/ft <sup>2</sup>

Ø80 µm

Depth: 85 µm

Surface copper: 12 µm

Dimple: <15 µm





## Via-Filling Performance at Tool A

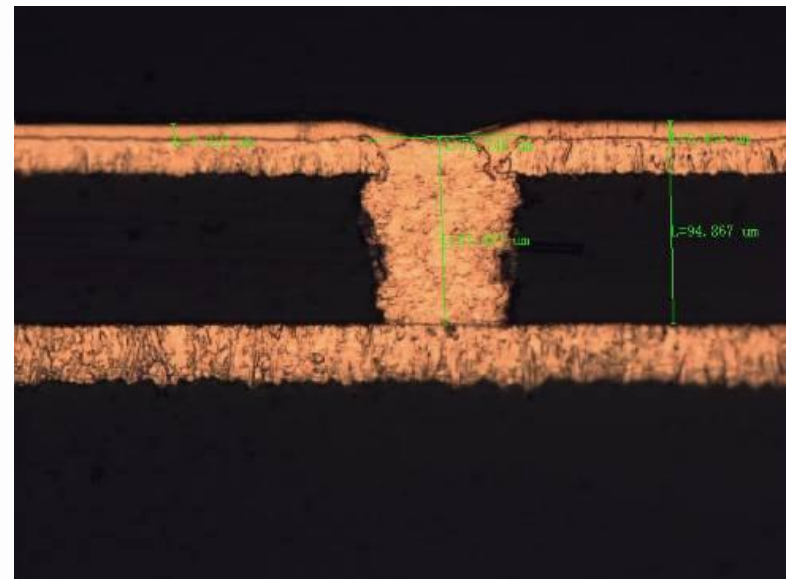
Conductivity Layer	Direct Metallization
Current density	1.5→2→2.5 ASD
Plating time	30 min
Sparger flowrate	10 L/ft <sup>2</sup>

Ø80 µm

Depth: 85 µm

Surface copper: 7 µm

Dimple: <15 µm



## Via-Filling Performance at Tool A

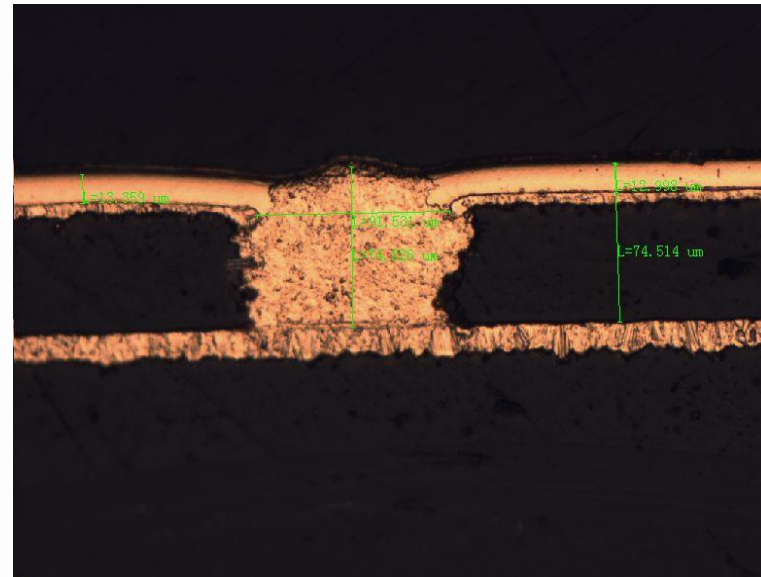
Conductivity Layer	Direct Metallization
Current density	2.5 → 1.5
Plating time	60 min
Sparger flowrate	10 L/ft <sup>2</sup>

Ø91 µm

Depth: 60 µm

Surface copper: 13 µm

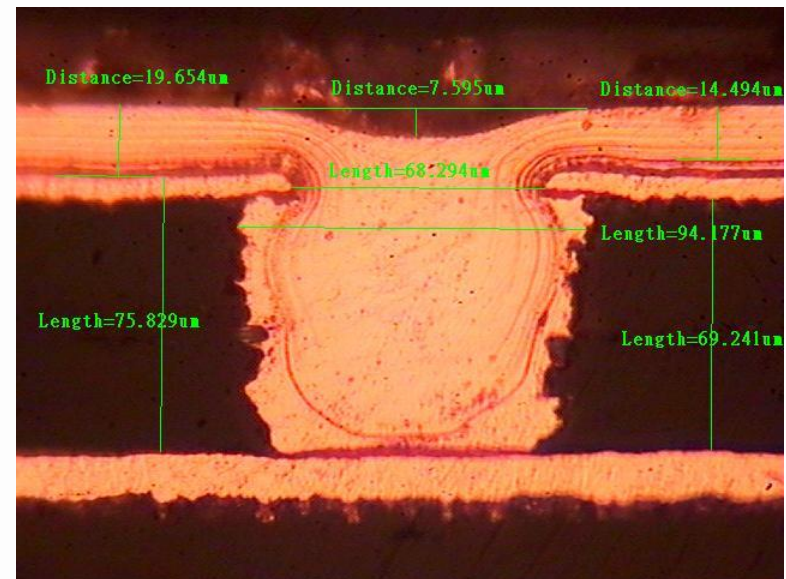
Dimple: ~0 µm



## Via-Filling Performance at Tool B

Conductivity Layer	Direct Metallization (with Flash)
Current density	2 ASD
Plating time	45 min
Sparger flowrate	0.2 bar

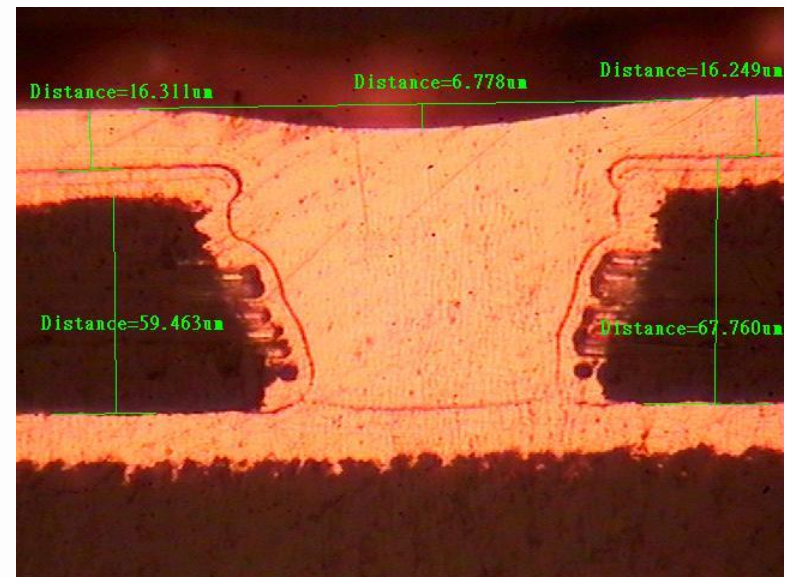
$\varnothing 90 \mu\text{m}$   
 Depth: 75  $\mu\text{m}$   
 Surface copper: 20  $\mu\text{m}$   
 Dimple: <8  $\mu\text{m}$



## Via-Filling Performance at Tool B

Conductivity Layer	Direct Metallization (with Flash)
Current density	1.5 ASD
Plating time	60 min
Sparger flowrate	0.3 bar

Ø95 µm  
 Depth: 65 µm  
 Surface copper: 16 µm  
 Dimple: <7 µm

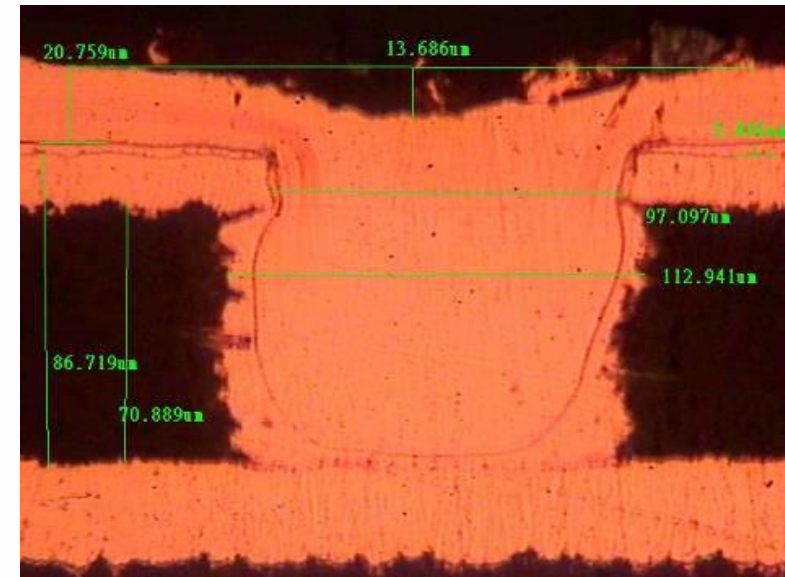




## Via-Filling Performance at Tool B

Conductivity Layer	Electroless Copper Flash
Current density	2.15 ASD (20 ASF)
Plating time	45 min
Sparger flowrate	0.1 bar

Ø4 mil  
 Depth: 3 mil  
 Surface copper: 20  $\mu\text{m}$   
 Dimple: ~13 $\mu\text{m}$



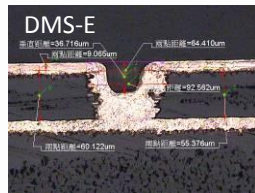


Via open / depth: 3 mils / 2 mils

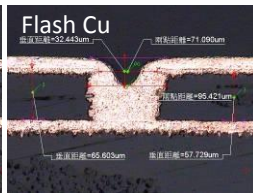
**Via Open/Depth: 3/2 mil**

**25 ASF**

Plated Cu thk:



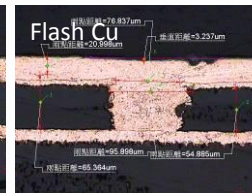
9.07um



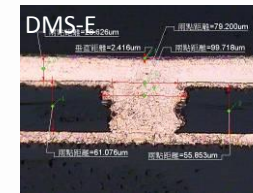
10.14um



20.99um



20.99um



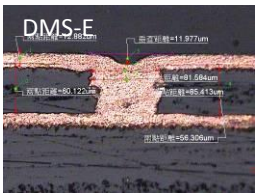
28.63um



32.0um

**20 ASF**

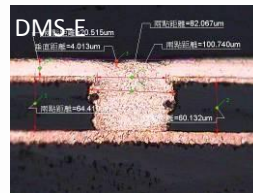
Plated Cu thk:



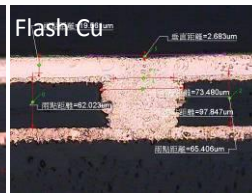
12.82um



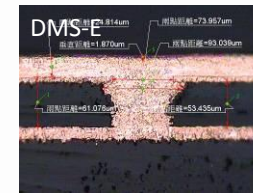
15.70um



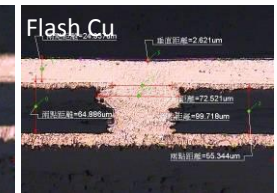
20.52um



19.58um



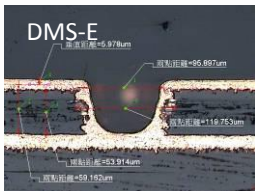
24.81um



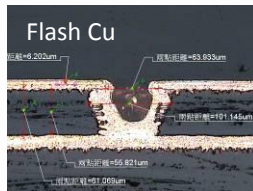
24.34um

**15 ASF**

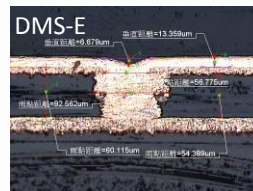
Plated Cu thk:



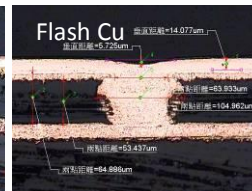
5.98um



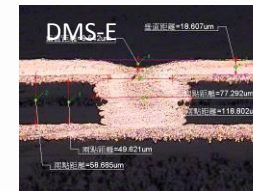
6.20um



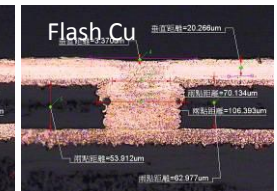
13.36um



14.08um



18.61um



20.27um

**20 min**

**40 min**

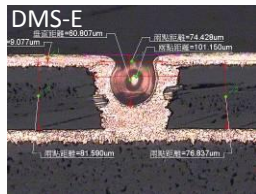
**60 min**

Via open / depth: 3 mils / 3 mils

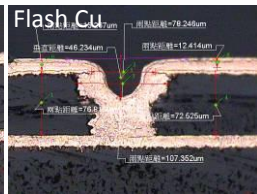
**Via Open/Depth: 3/3 mil**

**25 ASF**

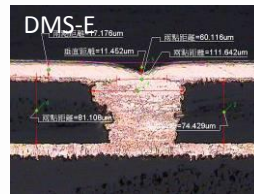
Plated Cu thk:



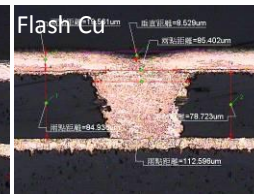
9.07um



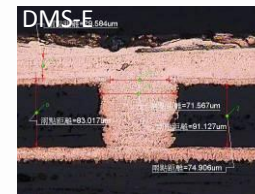
12.41um



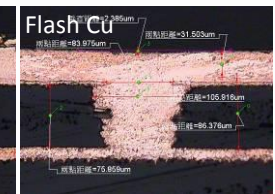
17.18um



19.56um



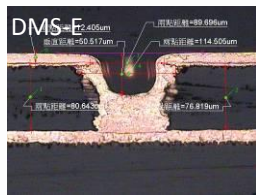
29.58um



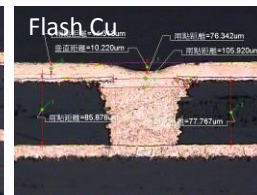
31.50um

**20 ASF**

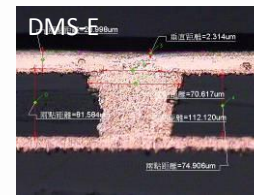
Plated Cu thk:



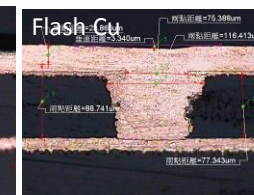
12.41um



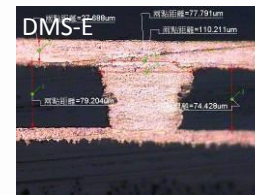
14.31um



21.00um



23.86um



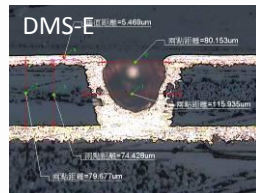
27.70um



25.77um

**15 ASF**

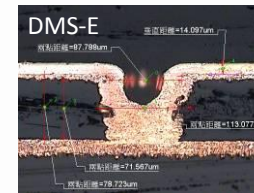
Plated Cu thk:



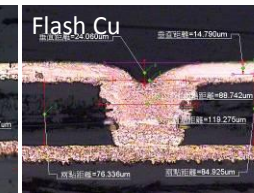
5.47um



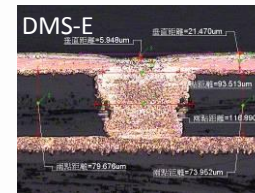
5.25um



14.10um



14.79um



21.47um



22.24um

**20 min**

**40 min**

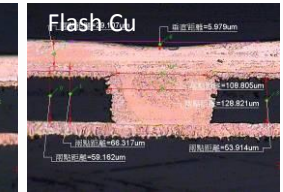
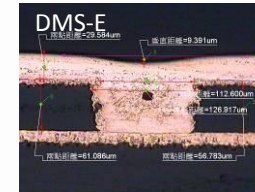
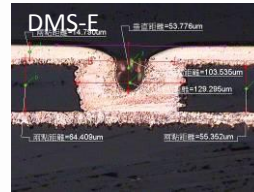
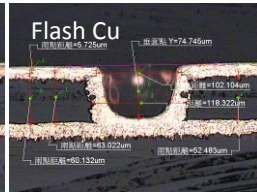
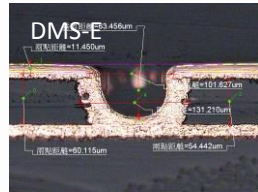
**60 min**



Via open / depth: 4 mils / 2 mils

**Via Open/Depth: 4/2 mil**

**25 ASF**



Plated Cu thk:

11.45um

5.73um

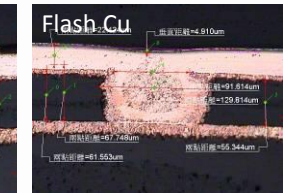
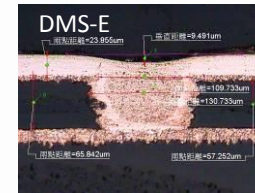
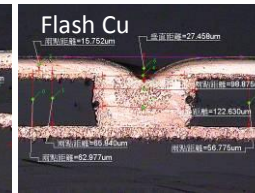
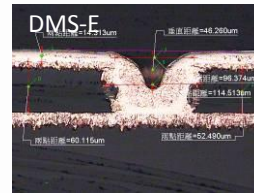
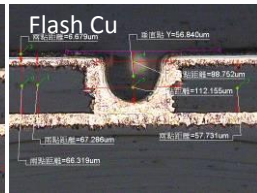
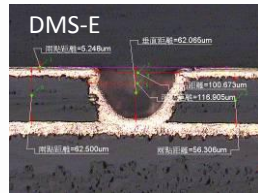
14.79um

17.65um

29.58um

29.12um

**20 ASF**



Plated Cu thk:

5.25um

6.68um

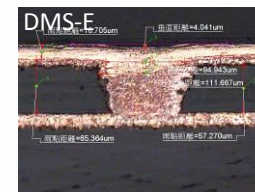
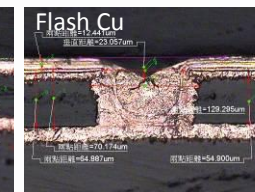
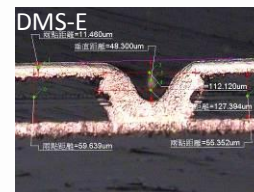
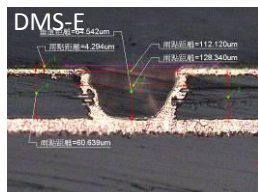
14.31um

15.75um

23.96um

22.42um

**15 ASF**



Plated Cu thk:

4.29um

6.20 um

11.46um

12.44um

16.71um

19.09um

**20 min**

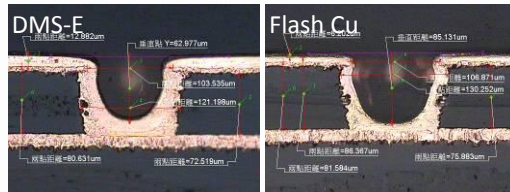
**40 min**

**60 min**

# Via Open/Depth: 4/3 mil

Via open / depth: 4 mils / 3 mils

**25 ASF**



Plated Cu thk:

12.88um

6.20um

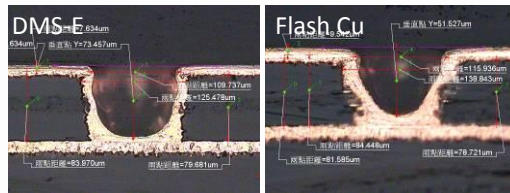
20.04um

21.47um  
(~90%)

28.64um

33.88um  
(~95%)

**20 ASF**



Plated Cu thk:

7.63um

9.54um  
(~100%)

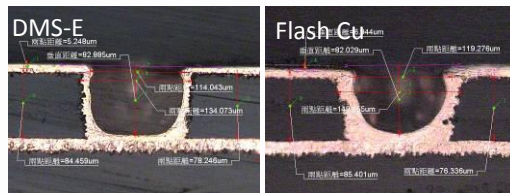
16.22um

16.70um  
(~88%)

24.33um

21.00um  
(~75%)

**15 ASF**



Plated Cu thk:

5.25um

6.94 um  
(~95%)

9.07um

13.36um  
(~95%)

17.18um

19.08um  
(~90%)

**20 min**

**40 min**

**60 min**



Samples were plated in different equipment build up Cu thickness. These panels were then multi-reflowed at 260+/-0° C. Resistance change of daisy chain was less than 2% after 10X reflow as shown below.

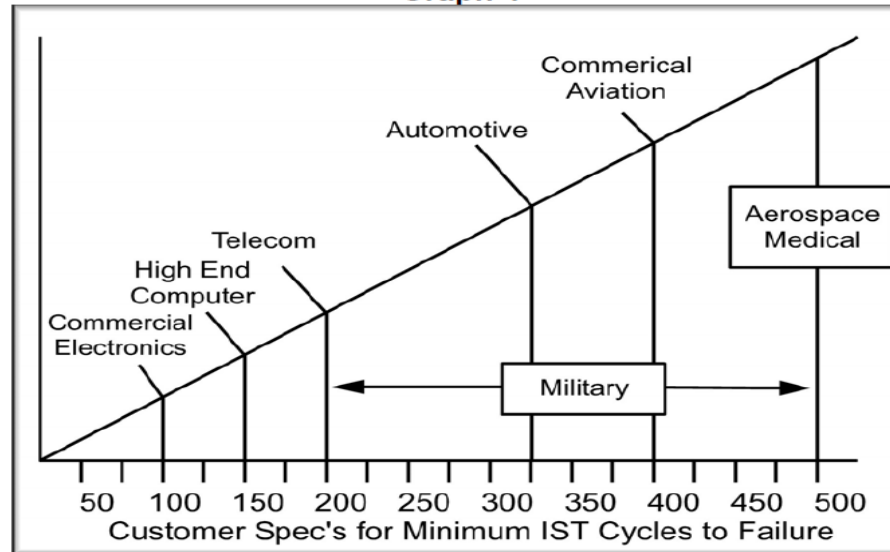
		before reflow						after reflow(260°C 10X Moto2)						change rate/ %					
		top			bottom			top			bottom			top			bottom		
		line 1	line 2	line 3	line 1	line 2	line 3	line 1	line 2	line 3	line 1	line 2	line 3	line 1	line 2	line 3	line 1	line 2	line 3
A	HDI daisy chain	Unit1	1.60	1.57	1.59	1.62	1.63	1.69	1.61	1.58	1.59	1.62	1.63	1.69	0.6%	0.6%	0.0%	0.0%	0.0%
		Unit2	1.53	1.46	1.46	1.55	1.55	1.62	1.53	1.47	1.46	1.56	1.57	1.64	0.0%	0.7%	0.0%	0.6%	1.3%
		Unit3	1.60	1.54	1.56	1.65	1.55	1.63	1.63	1.56	1.57	1.65	1.55	1.64	1.9%	1.3%	0.6%	0.0%	0.6%
		Unit4	1.48	1.45	1.50	1.58	1.49	1.57	1.49	1.45	1.50	1.58	1.50	1.58	0.7%	0.0%	0.0%	0.0%	0.6%
		Unit5	1.63	1.64	1.63	1.67	1.66	1.68	1.65	1.66	1.64	1.69	1.66	1.69	1.2%	1.2%	0.6%	1.2%	0.6%
		Unit6	1.56	1.54	1.53	1.63	1.60	1.64	1.56	1.54	1.56	1.64	1.61	1.64	0.0%	0.0%	2.0%	0.6%	0.6%
		Unit7	1.63	1.59	1.54	1.72	1.65	1.65	1.64	1.60	1.57	1.73	1.66	1.66	0.6%	0.6%	1.9%	0.6%	0.6%
		Unit8	1.53	1.50	1.47	1.67	1.59	1.59	1.54	1.51	1.48	1.68	1.59	1.59	0.7%	0.7%	0.7%	0.6%	0.0%
		Unit9	1.53	1.49	1.55	1.53	1.61	1.53	1.53	1.50	1.57	1.53	1.62	1.56	0.0%	0.7%	1.3%	0.0%	0.6%
		Unit10	1.54	1.49	1.52	1.58	1.57	1.60	1.54	1.50	1.53	1.58	1.58	1.61	0.0%	0.7%	0.7%	0.0%	0.6%
		Unit11	1.51	1.51	1.48	1.63	1.59	1.63	1.51	1.52	1.49	1.63	1.59	1.63	0.0%	0.7%	0.7%	0.0%	0.0%
		Unit12	1.49	1.48	1.49	1.65	1.59	1.58	1.49	1.48	1.49	1.65	1.60	1.61	0.0%	0.0%	0.0%	0.0%	1.9%
	through hole daisy chain	Unit13	1.45	1.41	1.46	1.60	1.60	1.68	1.45	1.42	1.46	1.61	1.61	1.70	0.0%	0.7%	0.0%	0.6%	1.2%
		Unit14	0.53	0.54	0.55	N/A			0.54	0.54	0.56	N/A			1.9%	0.0%	1.8%	N/A	
		Unit15	0.58	0.55	0.55				0.58	0.56	0.56				0.0%	1.8%	1.8%		
		Unit16	0.54	0.55	0.54				0.55	0.56	0.55				1.9%	1.8%	1.9%		
		Unit17	0.55	0.56	0.54				0.56	0.56	0.54				1.8%	0.0%	0.0%		
		Unit18	0.55	0.55	0.54				0.55	0.55	0.55				0.0%	0.0%	1.9%		
		Unit19	0.56	0.55	0.53				0.55	0.55	0.54				-1.8%	0.0%	1.9%		
B	HDI daisy chain	Unit1	1.72	1.71	1.77	1.64	1.63	1.68	1.74	1.72	1.80	1.64	1.64	1.69	1.2%	0.6%	1.7%	0.0%	0.6%
		Unit2	1.71	1.68	1.76	1.57	1.54	1.57	1.70	1.69	1.77	1.59	1.53	1.57	-0.6%	0.6%	0.6%	1.3%	-0.6%
		Unit3	1.77	1.75	1.75	1.67	1.64	1.70	1.79	1.76	1.74	1.69	1.66	1.72	1.1%	0.6%	-0.6%	1.2%	1.2%
		Unit4	1.73	1.75	1.74	1.60	1.56	1.63	1.71	1.76	1.77	1.61	1.59	1.64	-1.2%	0.6%	1.7%	0.6%	1.9%
		Unit5	1.84	1.78	1.80	1.74	1.73	1.74	1.86	1.79	1.81	1.74	1.73	1.74	1.1%	0.6%	0.6%	0.0%	0.0%
		Unit6	1.83	1.78	1.79	1.66	1.64	1.66	1.85	1.78	1.79	1.67	1.66	1.67	1.1%	0.0%	0.0%	0.6%	1.2%
		Unit7	1.81	1.79	1.87	1.73	1.65	1.66	1.83	1.79	1.88	1.73	1.65	1.67	1.1%	0.0%	0.5%	0.0%	0.6%
		Unit8	1.82	1.78	1.86	1.65	1.57	1.58	1.83	1.80	1.88	1.67	1.59	1.60	0.5%	1.1%	1.1%	1.2%	1.3%
		Unit9	1.71	1.75	1.76	1.80	1.77	1.78	1.72	1.76	1.77	1.81	1.78	1.78	0.6%	0.6%	0.6%	0.6%	0.0%
		Unit10	1.82	1.74	1.77	1.71	1.69	1.65	1.83	1.75	1.77	1.70	1.69	1.66	0.5%	0.6%	0.0%	-0.6%	0.6%
		Unit11	1.86	1.84	1.86	1.71	1.69	1.77	1.86	1.84	1.86	1.71	1.70	1.77	0.0%	0.0%	0.0%	0.0%	0.6%
		Unit12	1.88	1.82	1.89	1.72	1.65	1.64	1.88	1.83	1.90	1.72	1.65	1.65	0.0%	0.5%	0.5%	0.0%	0.6%
	through hole daisy chain	Unit13	1.86	1.80	1.85	1.70	1.64	1.68	1.85	1.80	1.85	1.71	1.66	1.70	-0.5%	0.0%	0.0%	0.6%	1.2%
		Unit14	0.69	0.68	0.69	N/A			0.70	0.68	0.69	N/A			1.4%	0.0%	0.0%	N/A	
		Unit15	0.69	0.67	0.67				0.70	0.67	0.67				1.4%	0.0%	0.0%		
		Unit16	0.68	0.67	0.67				0.68	0.68	0.67				0.0%	1.5%	0.0%		
		Unit17	0.69	0.68	0.66				0.69	0.68	0.67				0.0%	0.0%	1.5%		
		Unit18	0.69	0.69	0.70				0.69	0.70	0.70				0.0%	1.4%	0.0%		
		Unit19	0.72	0.70	0.69				0.72	0.70	0.69				0.0%	0.0%	0.0%		

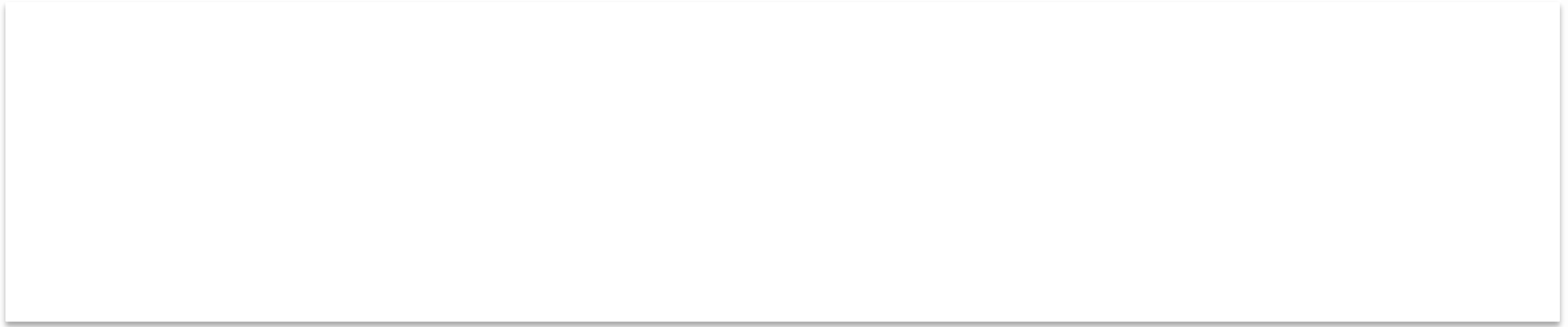


## IST Test Pass Over 500 Cycles

**IST Minimum Requirements by Industry** – IST testing is used in a number of industries. The graph below shows the typical minimum IST cycles to failure of coupons tested “As Received” (no preconditioning).

**Typical Minimum Requirement by Industry**  
**Graph 4**





### Observations and Considerations:

1. There were some “quality control” issues noted in this test set. One coupon arrived with an open on S1 and another with a short between P2/S2. Both defects were repaired. Reliability testing is best preformed on coupons that are free of quality related defects.
2. The IST cycles to failure mean of 293 may be somewhat lower than the average achieved testing similar coupons. The average of 20,781 coupons fabricated on a mid-range Tg material with a thickness between .062’ and .093” was 570 IST cycles to failure. A thinner coupon would be expected to surpass 570 cycles to failure.

Features	Benefits
<ul style="list-style-type: none"> <li>• Super Fills Blind Microvias (BMV)</li> </ul>	<ul style="list-style-type: none"> <li>• Higher productivity</li> <li>• Fewer process steps</li> <li>• Improved process yields</li> </ul>
<ul style="list-style-type: none"> <li>• Strong Filling Performance</li> </ul>	<ul style="list-style-type: none"> <li>• Exceptionally good filling               <ul style="list-style-type: none"> <li>▪ Typically &gt;100% &amp; dimple &lt; 5um</li> </ul> </li> <li>• Minimal surface copper deposited (&lt;15um)</li> </ul>
<ul style="list-style-type: none"> <li>• Short Plating Time for Via Fill (40-60 mins)</li> </ul>	<ul style="list-style-type: none"> <li>• High productivity</li> <li>• Lower labor cost</li> </ul>
<ul style="list-style-type: none"> <li>• Panel or Pattern Plate Processing Capability</li> </ul>	<ul style="list-style-type: none"> <li>• Process flexibility</li> <li>• Low surface copper thickness with excellent fill</li> </ul>
<ul style="list-style-type: none"> <li>• Insoluble anode</li> </ul>	<ul style="list-style-type: none"> <li>• Fast start up without dummy plating</li> <li>• Maintenance free</li> </ul>
<ul style="list-style-type: none"> <li>• No Pre-dip Bath</li> </ul>	<ul style="list-style-type: none"> <li>• No extra bath maintenance</li> </ul>
<ul style="list-style-type: none"> <li>• "All in one" system</li> </ul>	<ul style="list-style-type: none"> <li>• Accurate CVS control of plating bath additive</li> </ul>
<ul style="list-style-type: none"> <li>• Via Fill Process directly after Direct Metallization</li> </ul>	<ul style="list-style-type: none"> <li>• No additional flash copper plating</li> </ul>
<ul style="list-style-type: none"> <li>• Compatible with different equipment configuration</li> </ul>	<ul style="list-style-type: none"> <li>• Drop-in process for existing production lines</li> <li>• Low start-up cost</li> </ul>



NEW IDEAS ... FOR NEW HORIZONS

MARCH 25-27, 2014

MANDALAY BAY RESORT AND  
CONVENTION CENTER

LAS VEGAS, NEVADA

THE END!

THE END!